

# ***Assessment of Carbon Capture and Sequestration Options for Power Plants***

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**Illinois State Geological Survey**

*Clean Coal Study Group Meeting  
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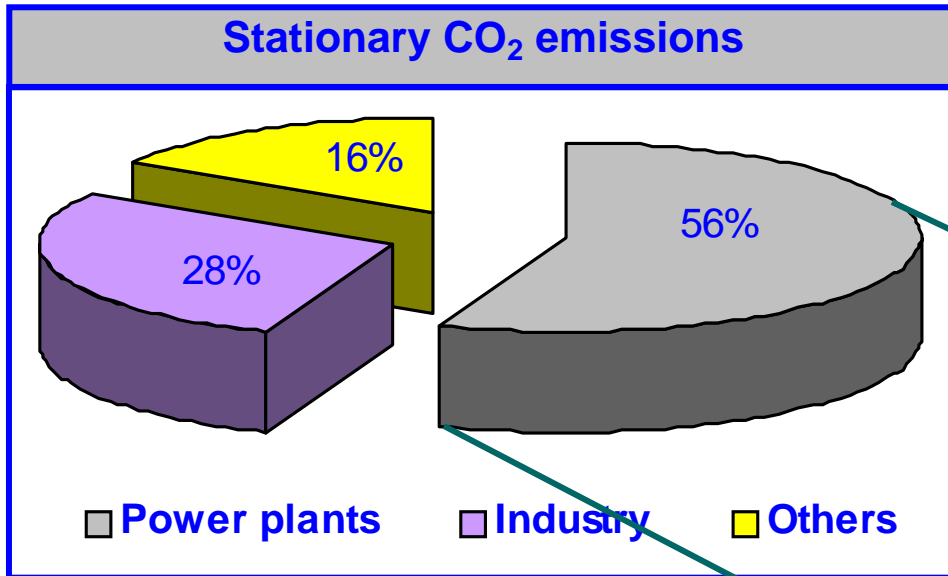
# Major Objectives of Phase I CO<sub>2</sub> Capture Task

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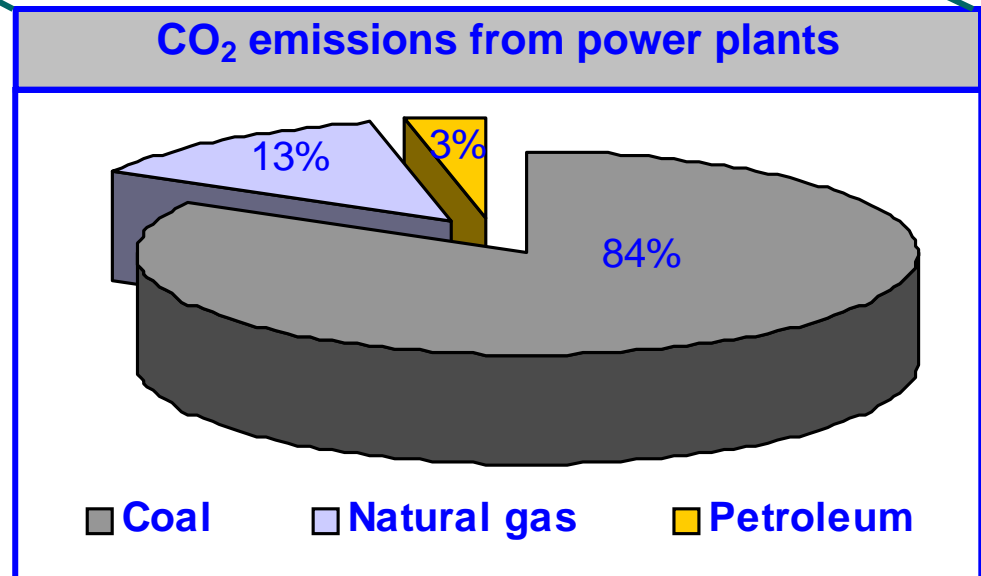
- ❑ *CO<sub>2</sub> emission sources in Illinois Basin*
- ❑ *Technical evaluation of CO<sub>2</sub> capture technologies for different emission sources*
- ❑ *Techno-economic analysis of CO<sub>2</sub> capture technologies*
- ❑ *Optimization of integrated capture, transportation and storage options*

# Annual CO<sub>2</sub> Emissions in the U.S. (in 2002)



□ All sources = 5,782 Mt

□ Stationary sources = 4,018 Mt (70%)

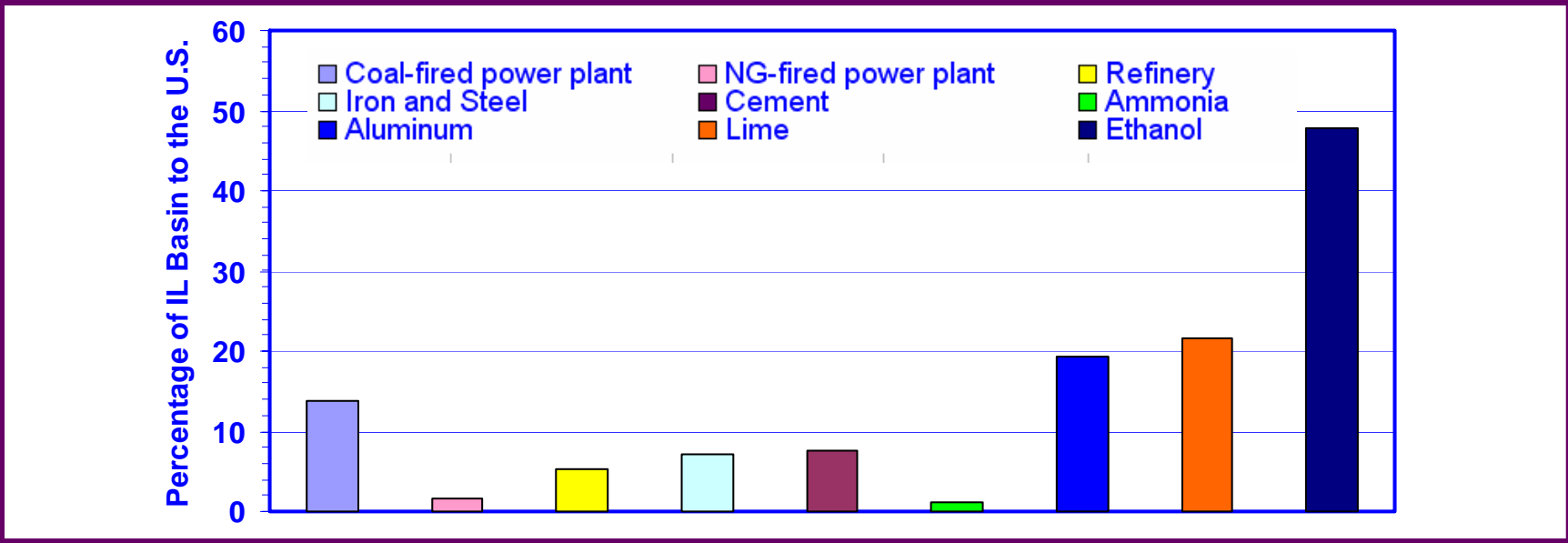
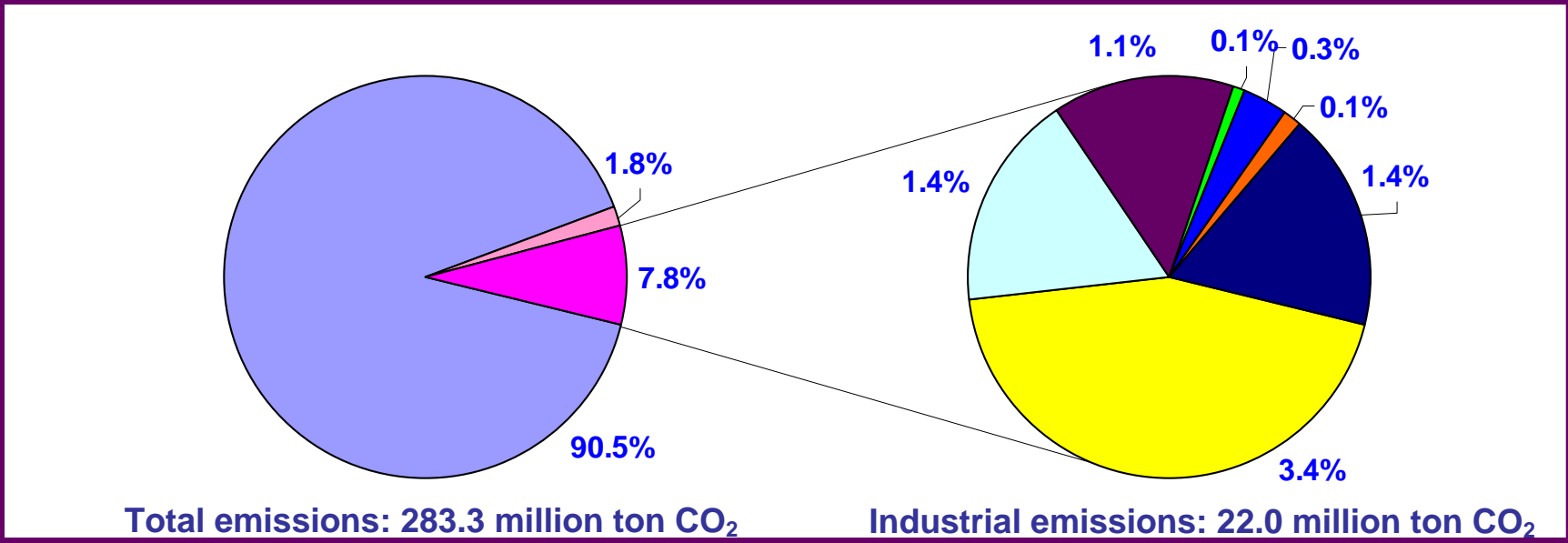


□ Coal-fired power plants = 1,868 Mt

➤ 32% of all sources

➤ 47% of stationary sources

# CO<sub>2</sub> Emissions in Illinois Basin

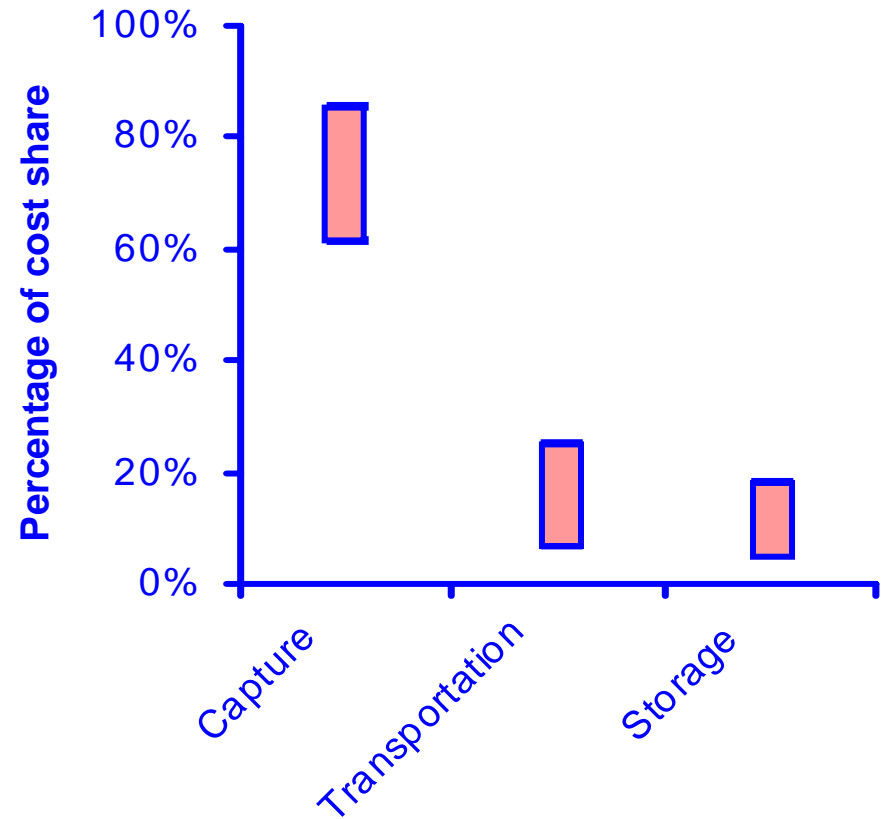
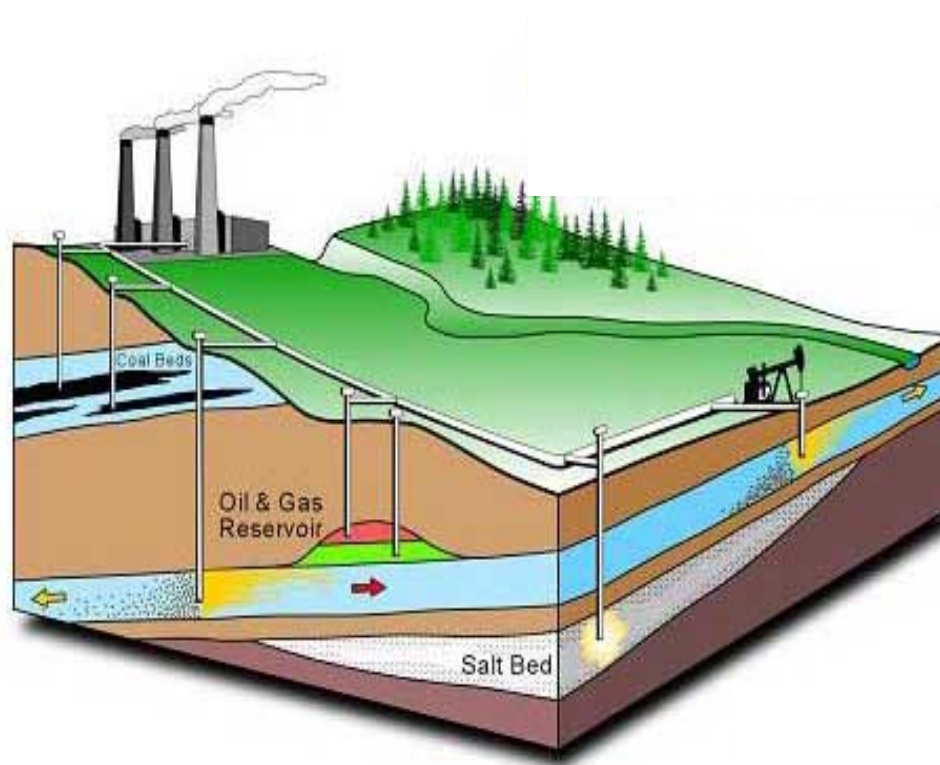


# CO<sub>2</sub> Concentrations in Flue Gases



<b>Source</b>	<b>CO<sub>2</sub> concentration (vol.%)</b>
<i>PC power station flue gas</i>	<b>14</b>
<i>Iron and steel blast furnace gas</i>	<b>20-27</b>
<i>Cement kiln off-gas</i>	<b>13-33</b>
<i>Lime manufacturing</i>	<b>13-33</b>
<i>Ammonia</i>	<b>&gt;95</b>
<i>Oil refinery</i>	<b>8-15</b>
<i>Ethanol Plants</i>	<b>&gt;85</b>

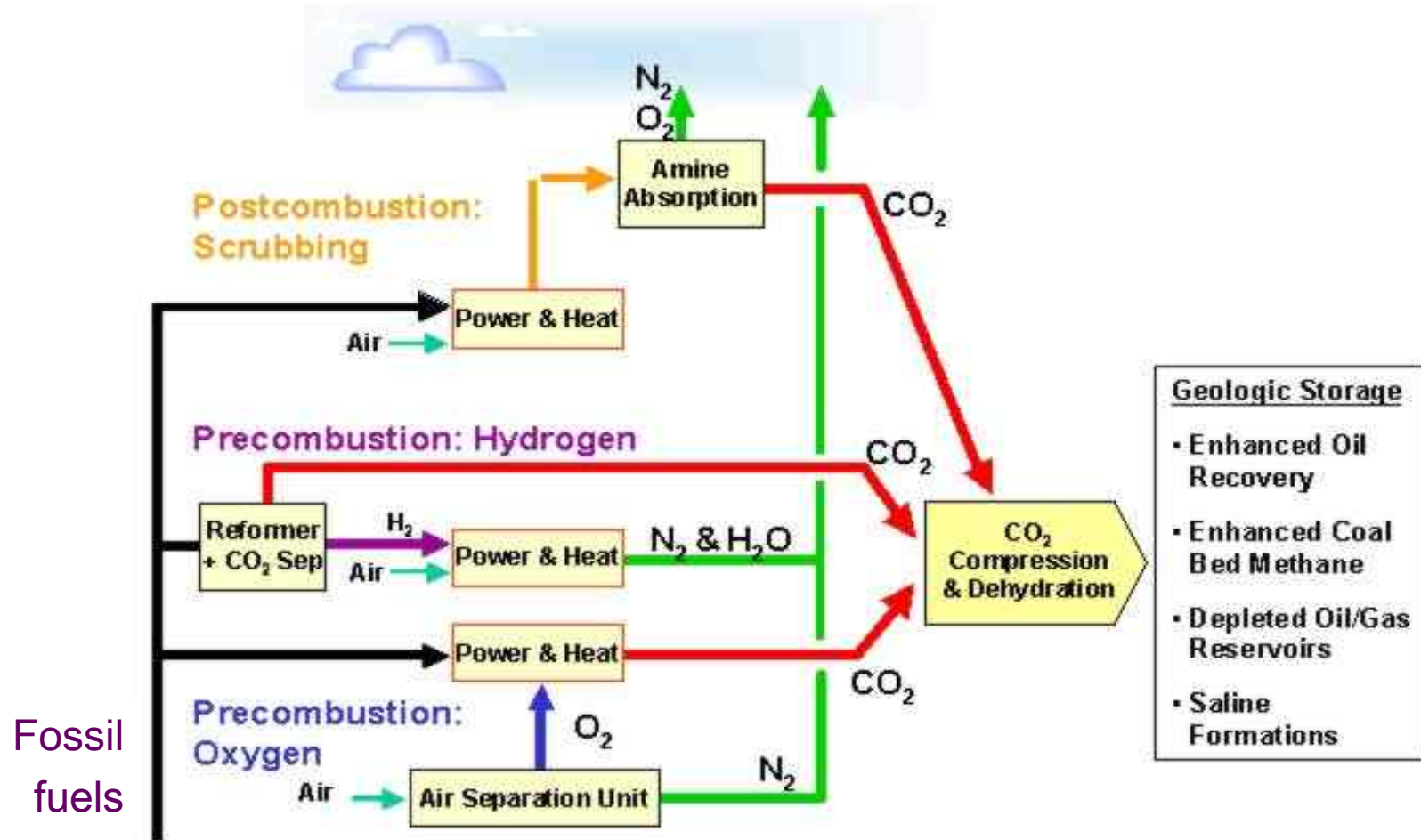
# Cost Breakdown in CO<sub>2</sub> Sequestration



## Cost assumptions:

- Capture: \$40-60/t CO<sub>2</sub> avoided
- Pipeline: \$0.02-0.06/t .km
- Transportation mileage: 250 km
- Storage: \$5-10/t CO<sub>2</sub>

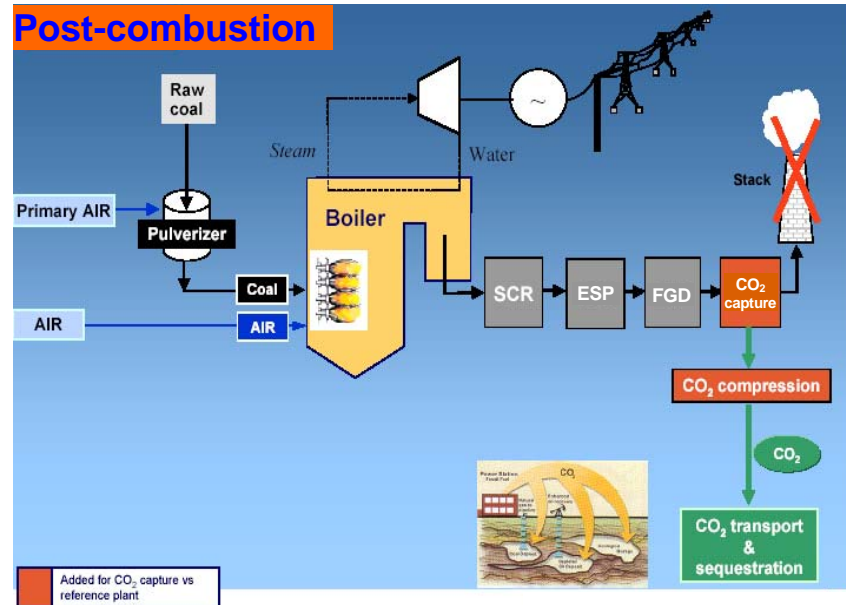
# Configurations for CO<sub>2</sub> Capture



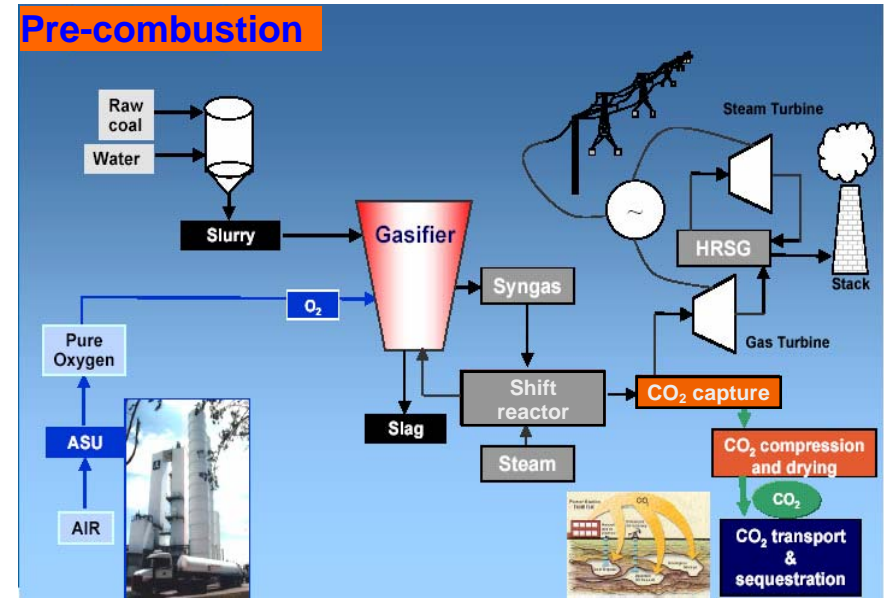
Info source: <http://www.co2captureproject.org/technologies/index.htm>

# Configurations for CO<sub>2</sub> Capture

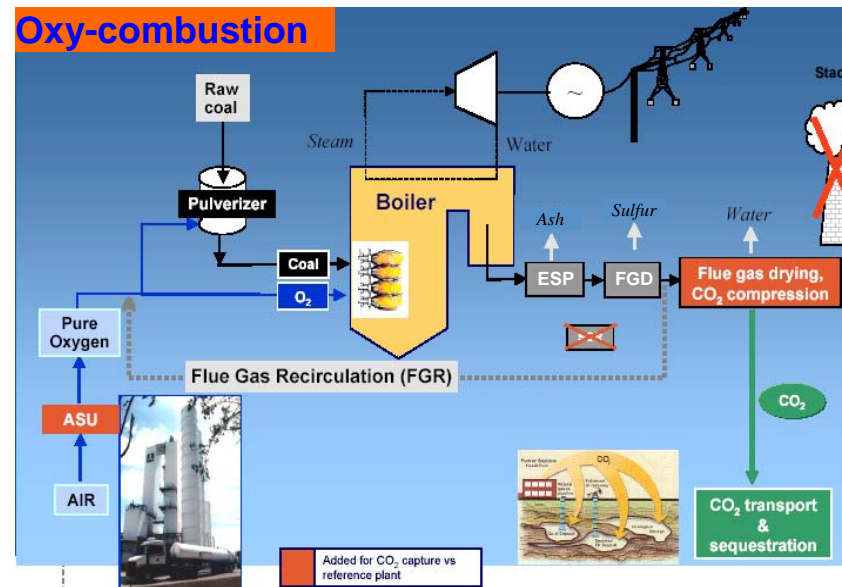
## Post-combustion



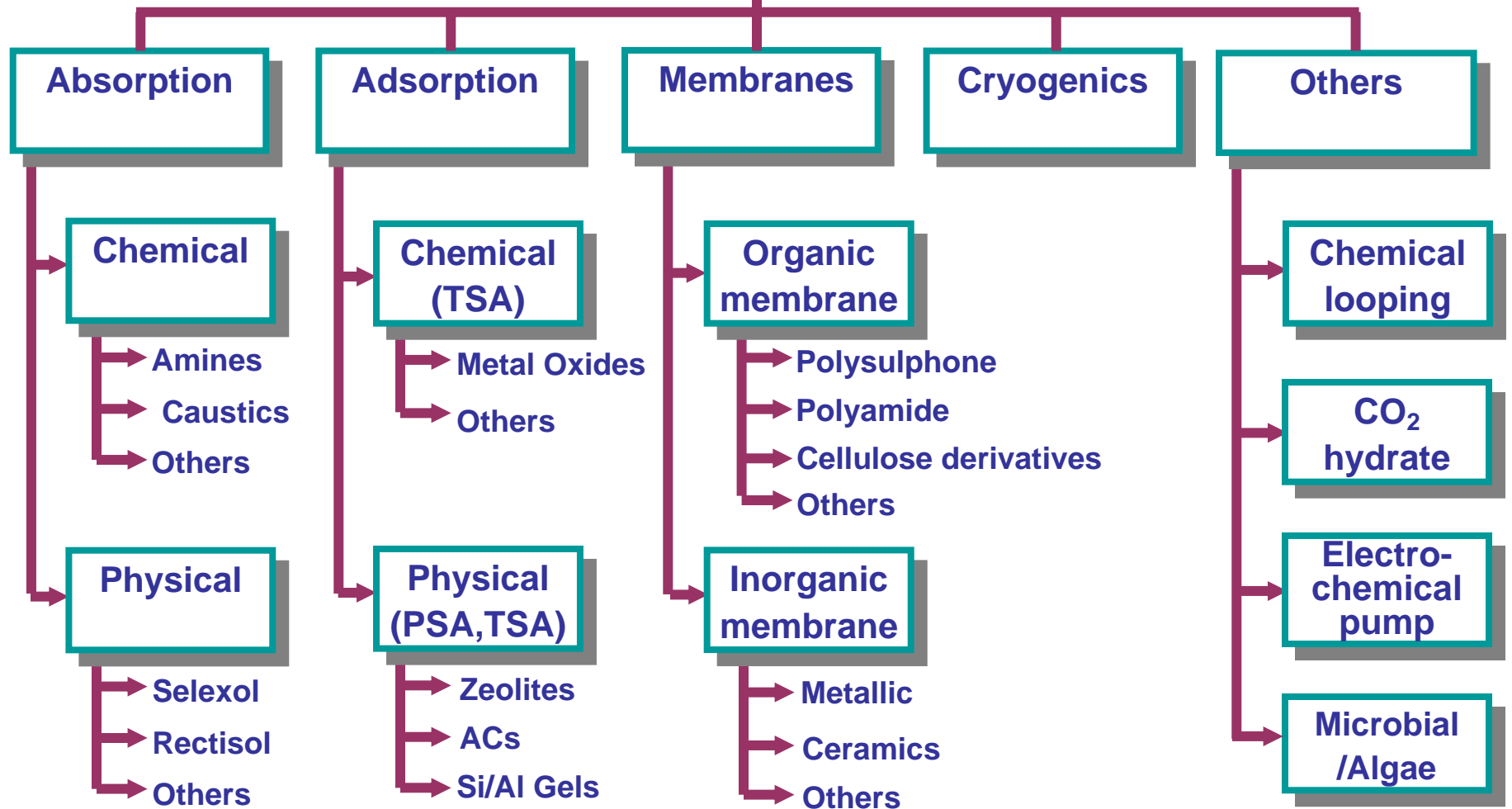
## Pre-combustion



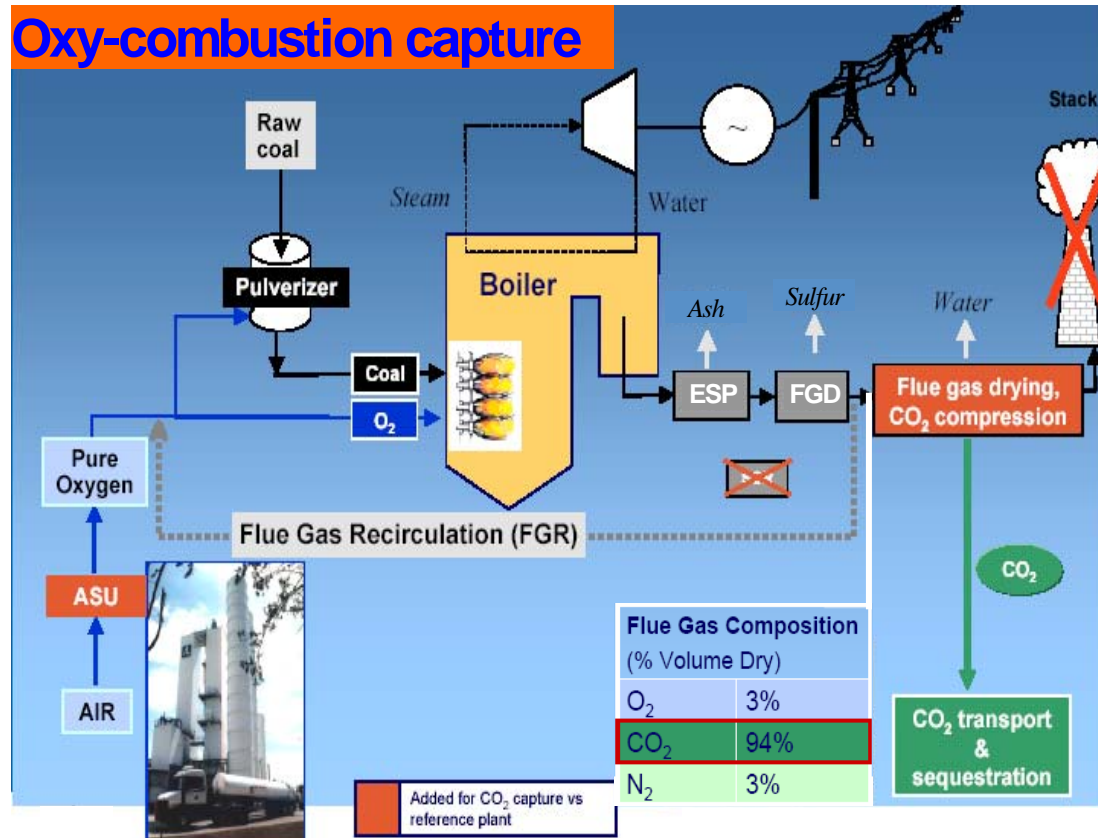
## Oxy-combustion



# Technologies for CO<sub>2</sub> Capture



# Oxy-Combustion



## □ Pilot-tests

- 94% CO<sub>2</sub> (dry) compared to 15% in air-blown combustion (AC)
- Flue gas volume 80% lower than AC
- 60 to 70% NO<sub>x</sub> reduction (0.08 to 0.1 lb/MM Btu)
- Compact design for new boilers

## □ No commercial operations

# Candidate CO<sub>2</sub> Capture Technologies



Source Type	Point of Capture	Amine Scrubbing	Ammonia Scrubbing	Physical Absorption	Gas Separation Membrane	Gas Absorption Membrane	Hydrate Formation	Oxyfuel + Drying/Compression
Power Plants Post-Combustion	Flue Gas	L	A	--	A	A	--	A
Power Plants Pre-Combustion	Shifted Syngas	--	--	L	A	--	A	--
Iron / Steel Facilities	Blast Furnace Gas (~60-70% of total CO <sub>2</sub> )	L	--	L	A	S	S	--
Refineries	Heater/Boiler Flue Gas (~65-85% of total CO <sub>2</sub> )	L	S	--	A	S	--	A
Cement Plants	Kiln Flue Gas	L	S	--	S	S	--	S

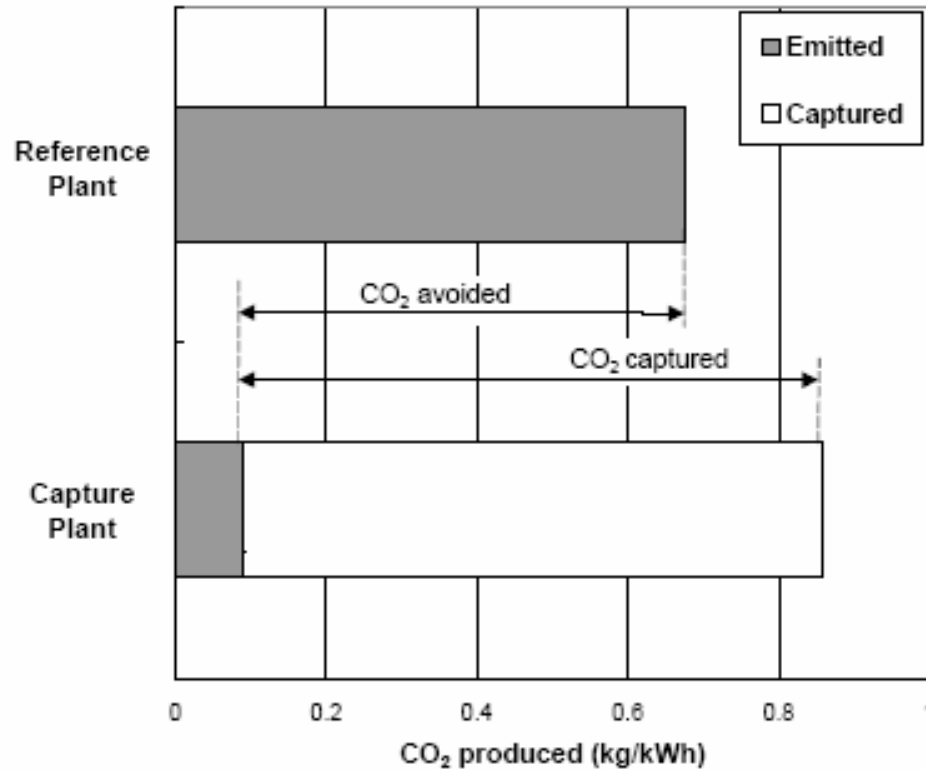
**Likely (L); Attractive (A); Speculative (S)**

# ***Techno-Economic Analysis***

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- Air-blown PC plant + chemical absorption process (MEA)*
- IGCC + shift + physical absorption process (Selexol)*
- Oxy-combustion*

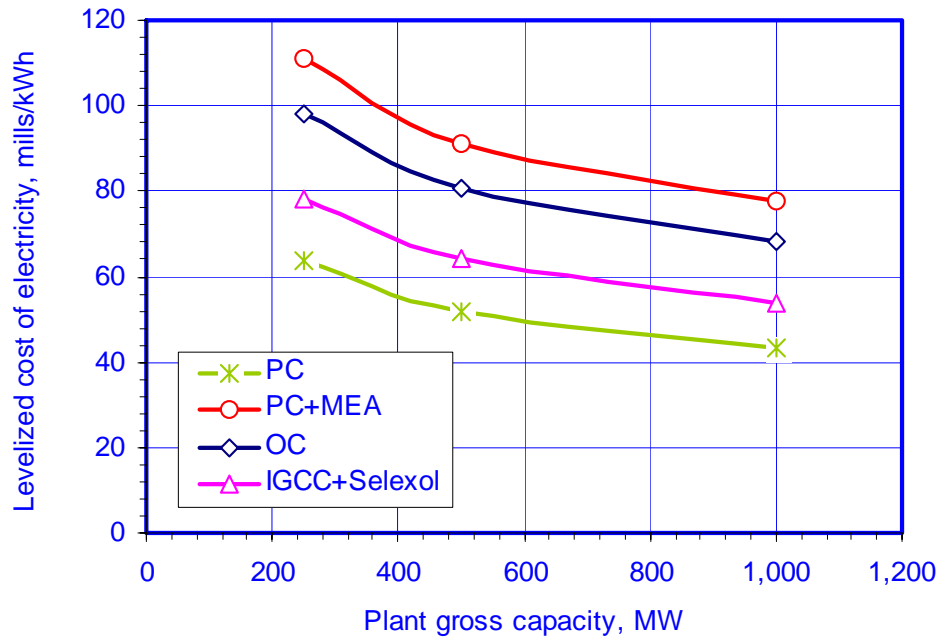
# CO<sub>2</sub> Avoidance and CO<sub>2</sub> Capture



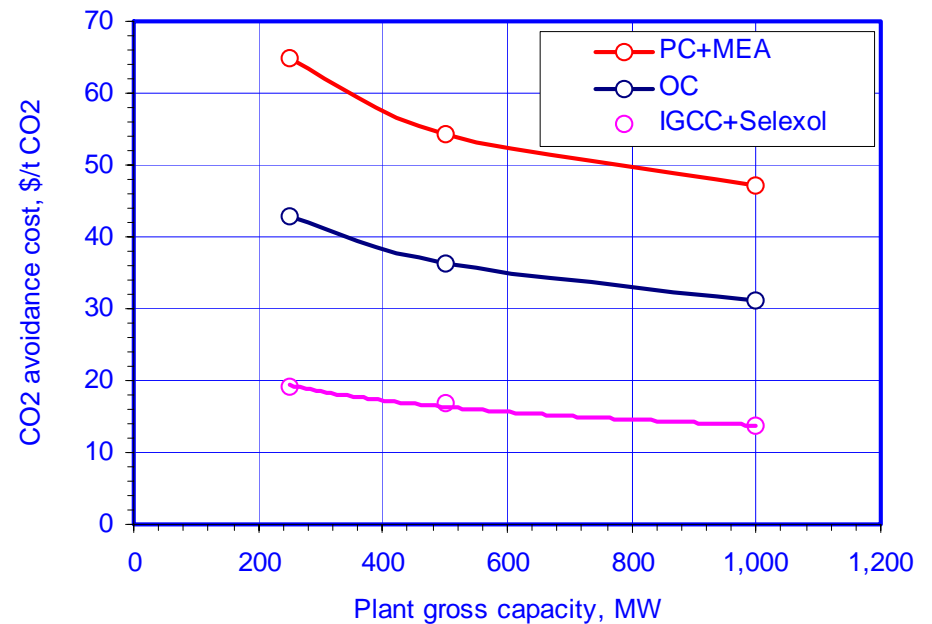
*Cost of CO<sub>2</sub> avoidance =  $\Delta$  cost of electricity / CO<sub>2</sub> avoided*

*Cost of CO<sub>2</sub> capture =  $\Delta$  cost of electricity / CO<sub>2</sub> captured*

# Costs of New Power Plants (IL coal)

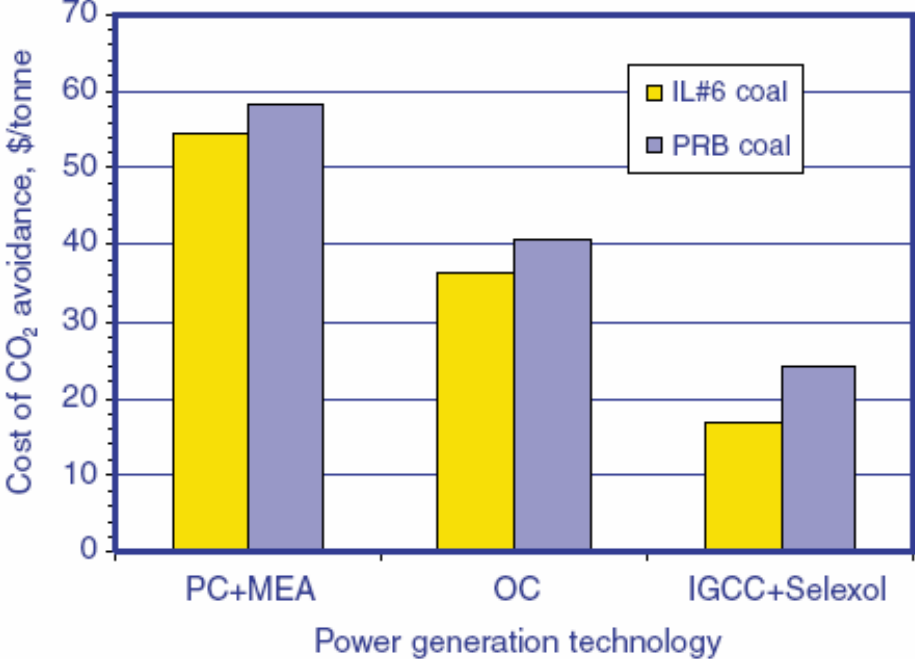
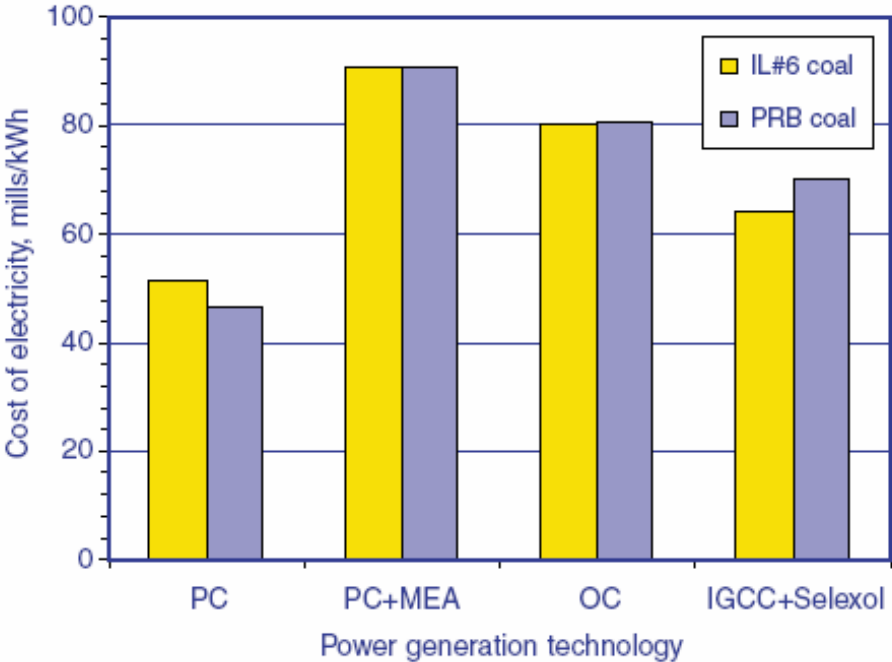


*Cost of electricity*



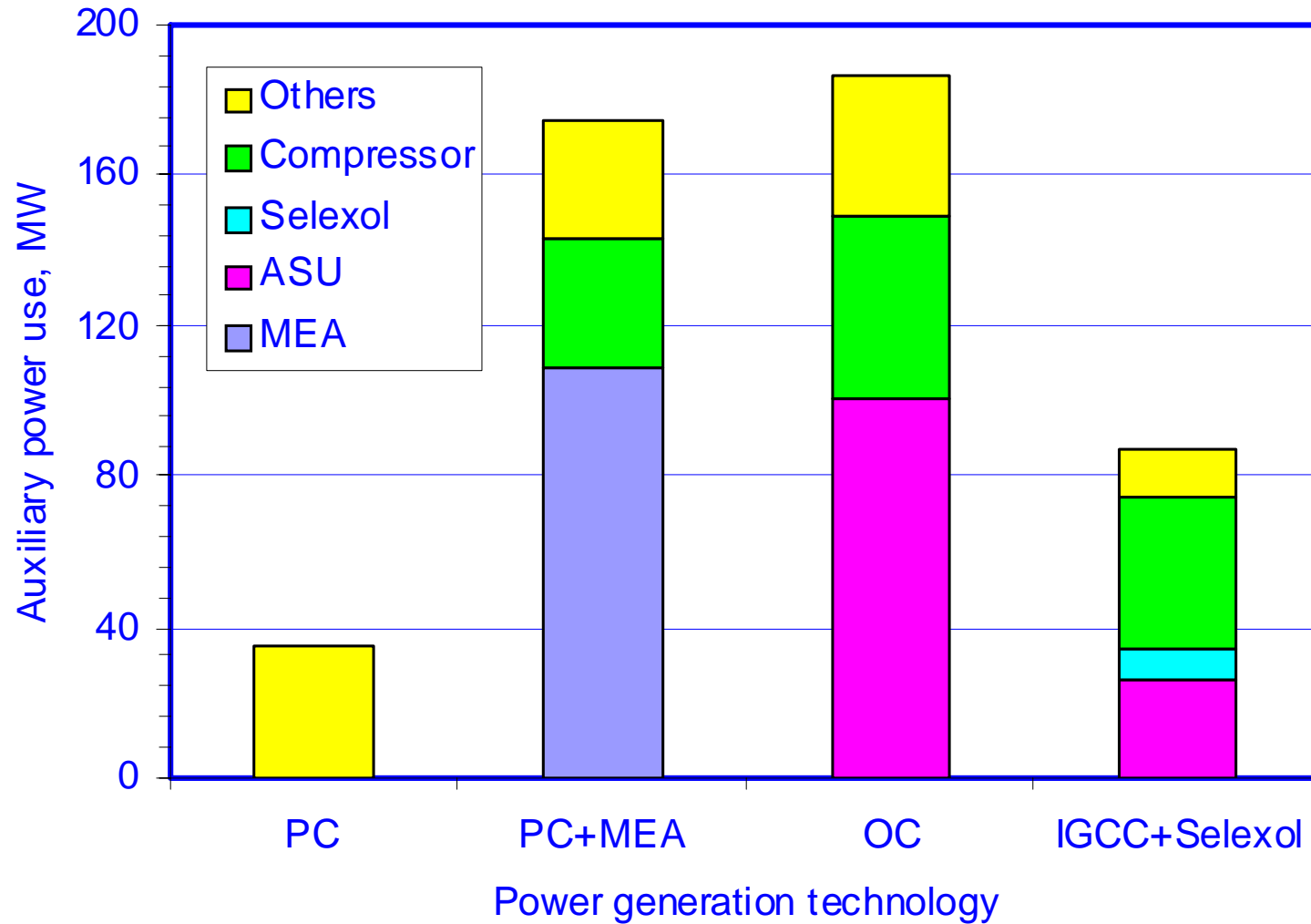
*CO<sub>2</sub> avoidance cost*

# Cost Comparison between IL Coal and PRB Coal



# Electricity Loss of New Power Plants (IL coal)

*Auxiliary power use of a 533 MW (gross) power plant*



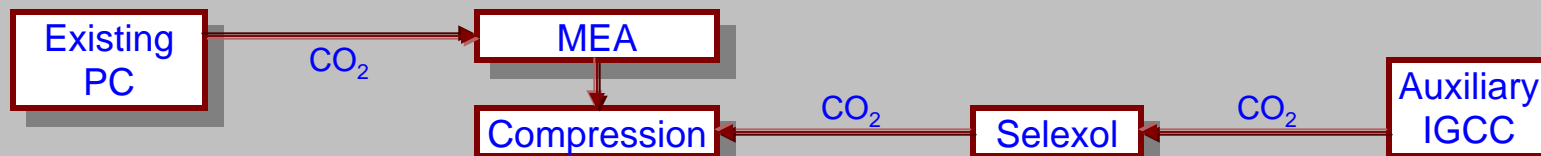
# CO<sub>2</sub> Capture Retrofit of Existing Plants: Case Studies



Case 1: MEA retrofit + auxiliary PC with MEA



Case 2: MEA retrofit + auxiliary NGCC w/o CO<sub>2</sub> capture



Case 3: MEA retrofit + auxiliary IGCC with Selexol

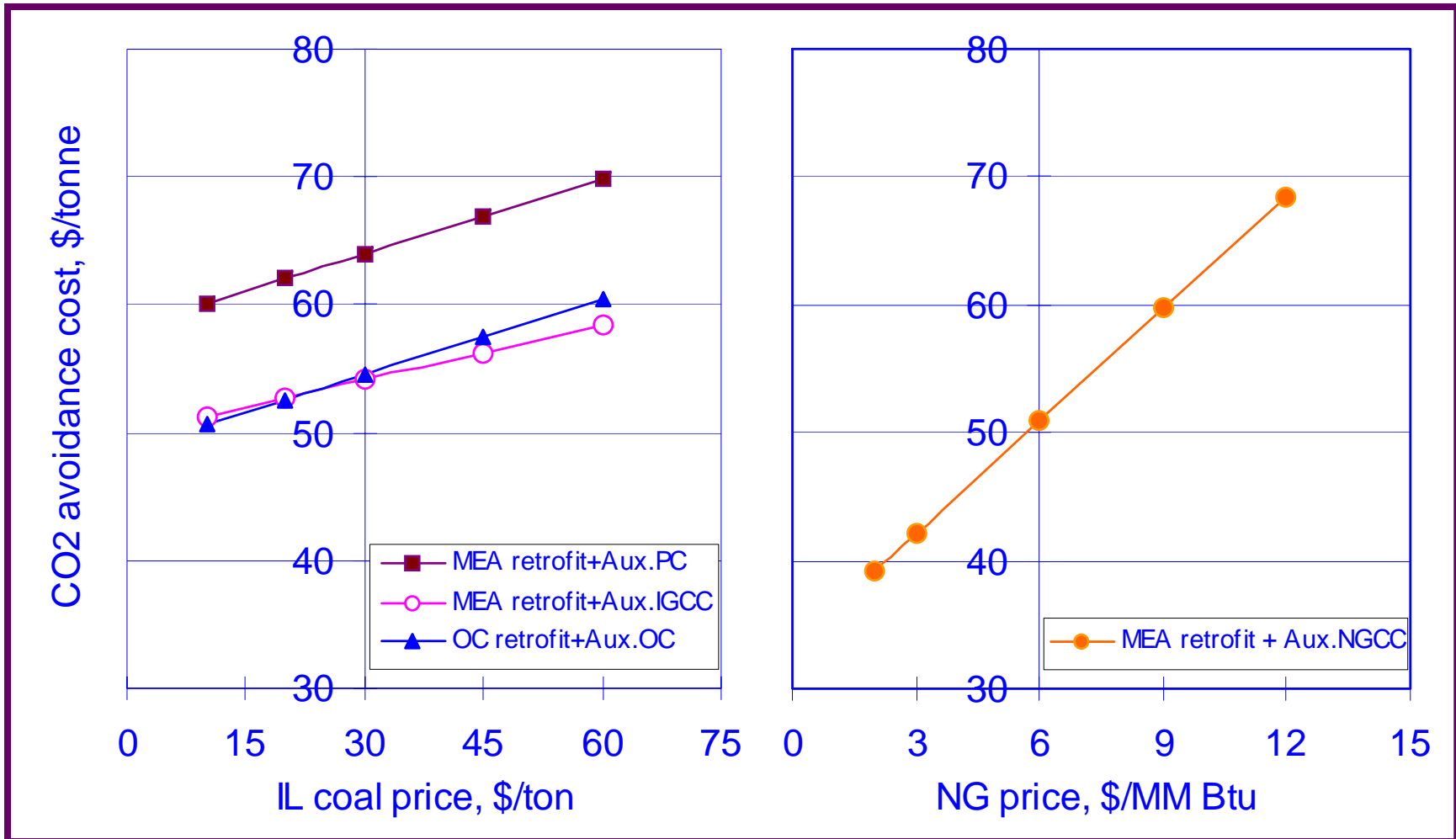


Case 4: Oxy-combustion (OC) retrofit + auxiliary OC

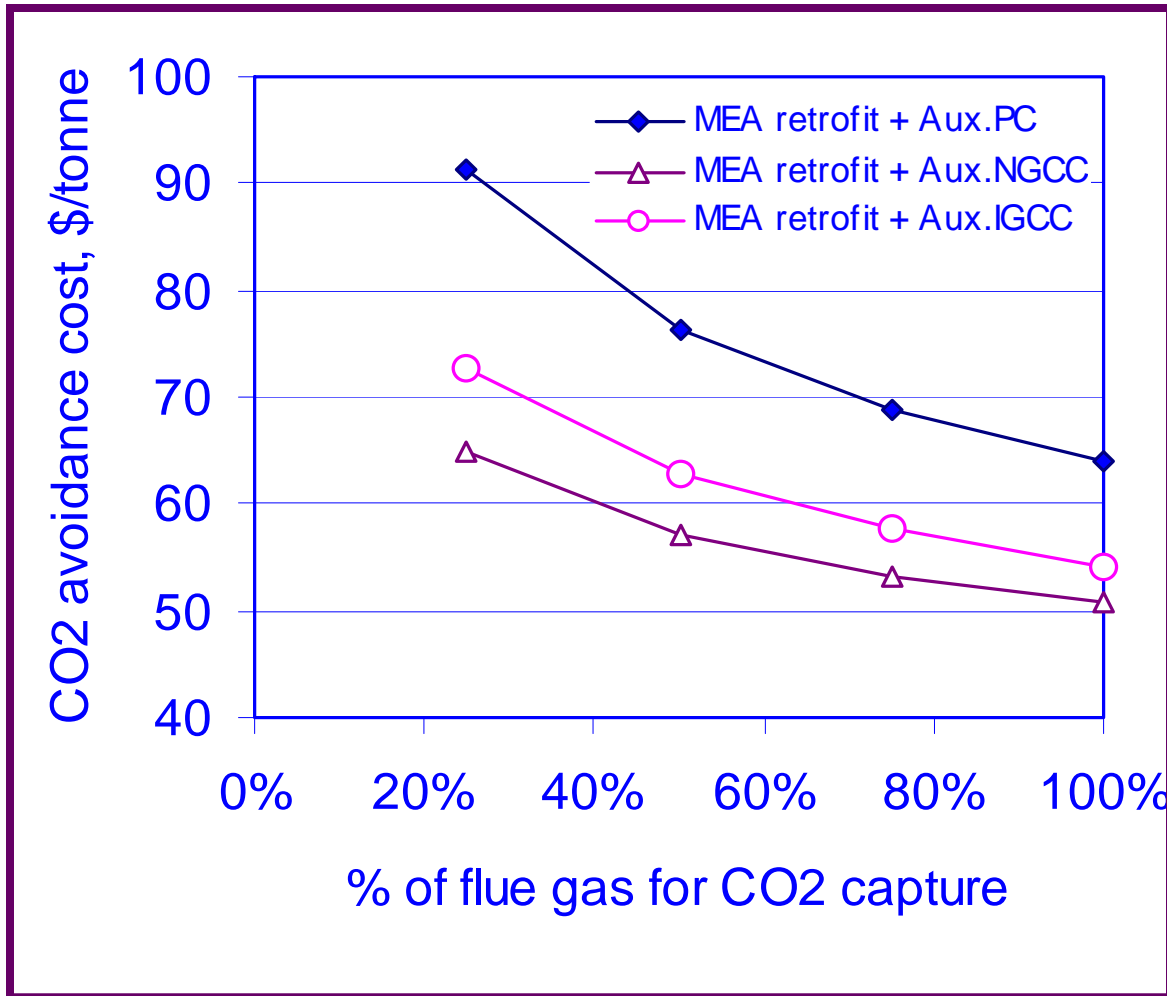
# Costs of Power Plant Retrofit



## Impact of fuel price



## Impact of retrofit scale



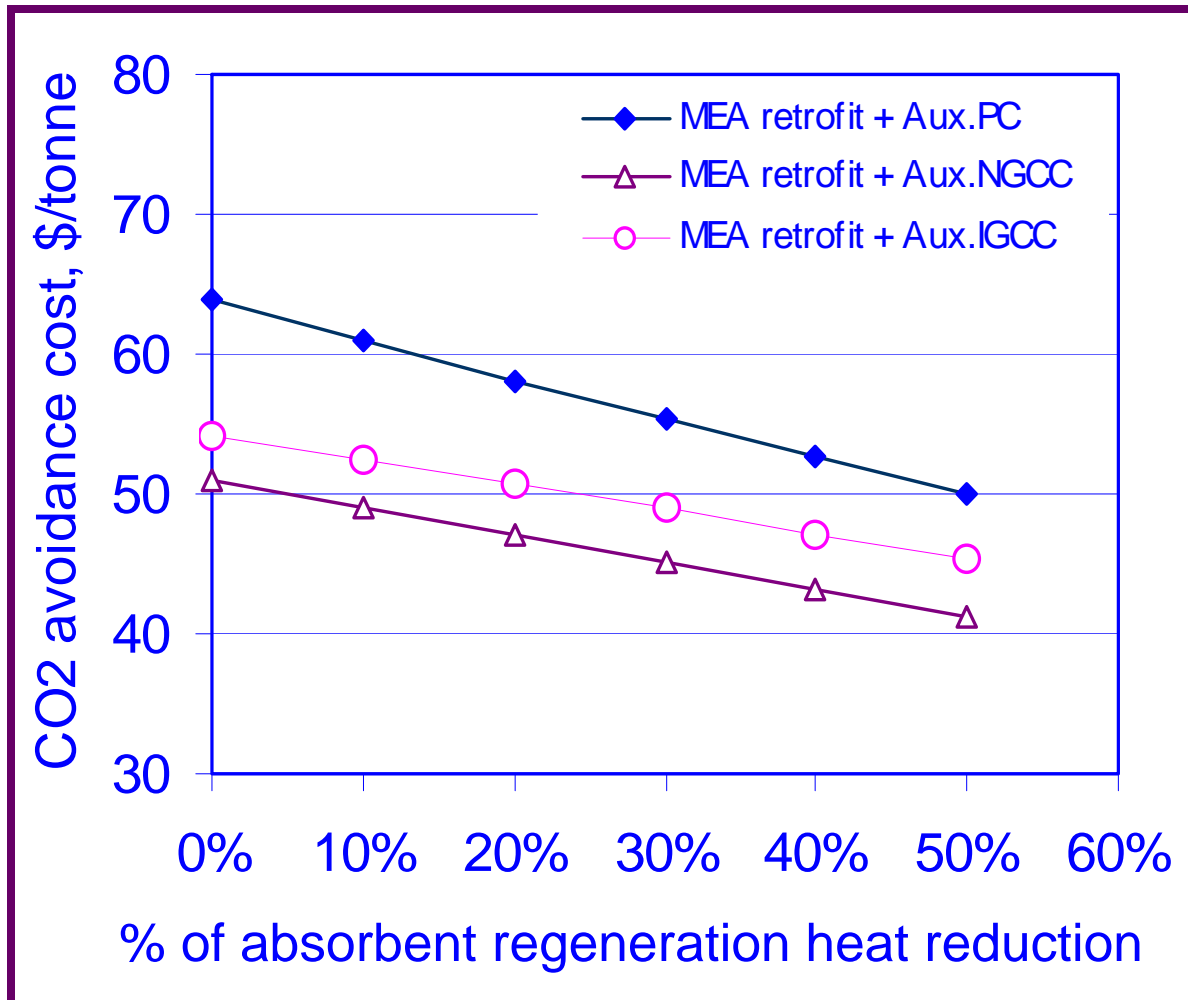
*equiv. power plant size*

**20%: 100MW**

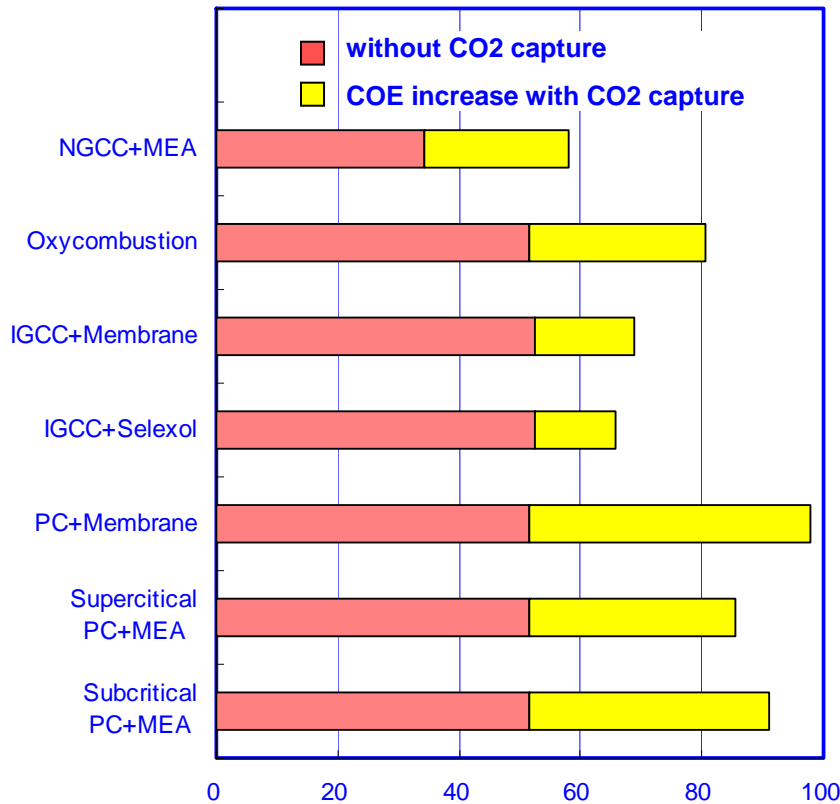
**50%: 250MW**

**100%: 500MW**

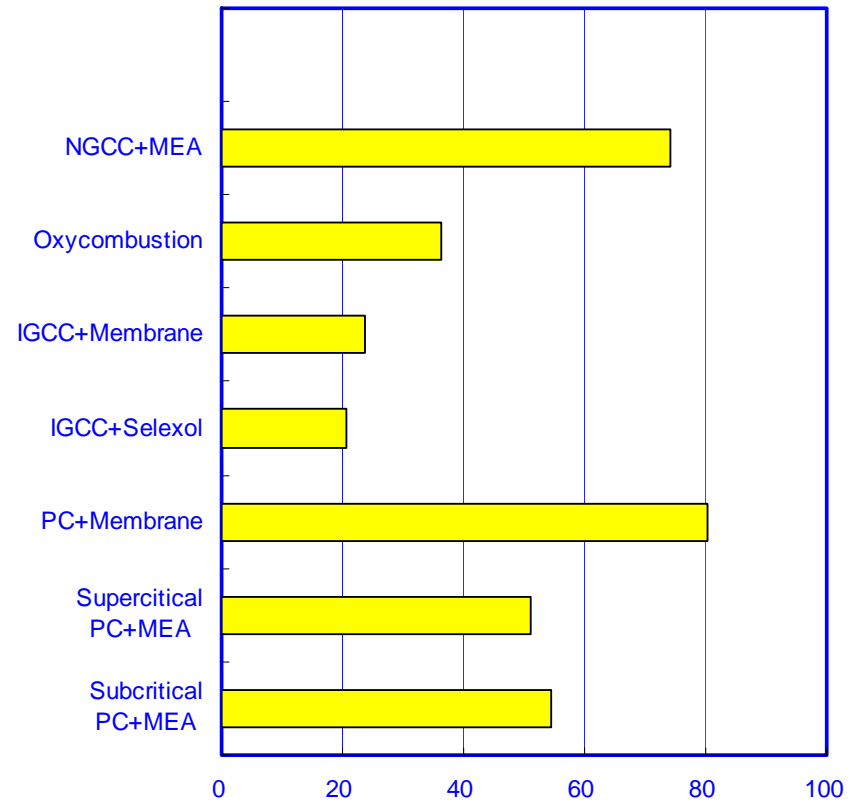
## Impact of chemical desorption heat



# Cost Comparison of Potential Technologies



Cost of electricity, mills/kWh



CO2 avoidance cost, \$/t

(All data in 2000 dollar; PC+ Membrane: 80% CO<sub>2</sub> recovery and 68% purity)

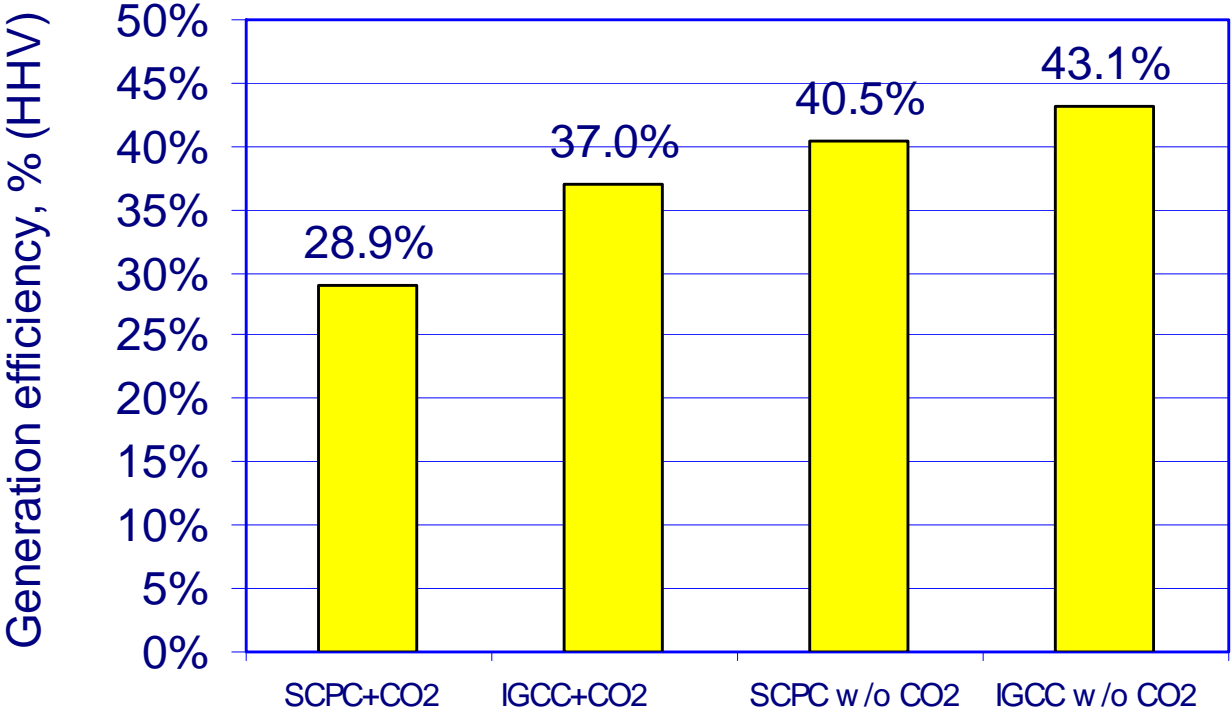
## Data sources:

1. Hendriks C., Carbon Dioxide Removal from Coal-fired Power Plants, Kluwer Academic Publishers, The Netherlands, 1994.
2. Parsons Energy and Chemicals Group Inc., Evaluation of Innovative Fossil Fuel Power Plants with CO<sub>2</sub> Removal, DOE Interim Report 1000316, 2002
3. Chen S.G., Lu Y. and Rostam-Abadi M., Assessment of Geological Carbon Sequestration Options in the Illinois Basin - Task 2: Assess Carbon Capture Options for Illinois Basin Carbon Dioxide Sources, DE-FC26-03NT41994, March 2005.

# Comparison between Super-Critical PC and IGCC



## Electricity generation efficiency, %



*Data source: Parsons Energy and Chemicals Group Inc., Evaluation of Innovative Fossil Fuel Power Plants with CO2 Removal, DOE Interim Report 1000316, 2002*

# Comparison between Super-Critical PC and IGCC



## Environmental emissions

	<i>lb/MM Btu (HHV)</i>		<i>lb/MWh</i>	
SO <sub>2</sub>	0.086	<i>neg.</i>	1.01	<i>neg.</i>
NO <sub>x</sub>	0.157	<0.028	1.85	0.25
PM	0.01	<i>neg.</i>	0.12	<i>neg.</i>
CO <sub>2</sub>	203*/20.2**	200/21.4	1707/237	1582/162

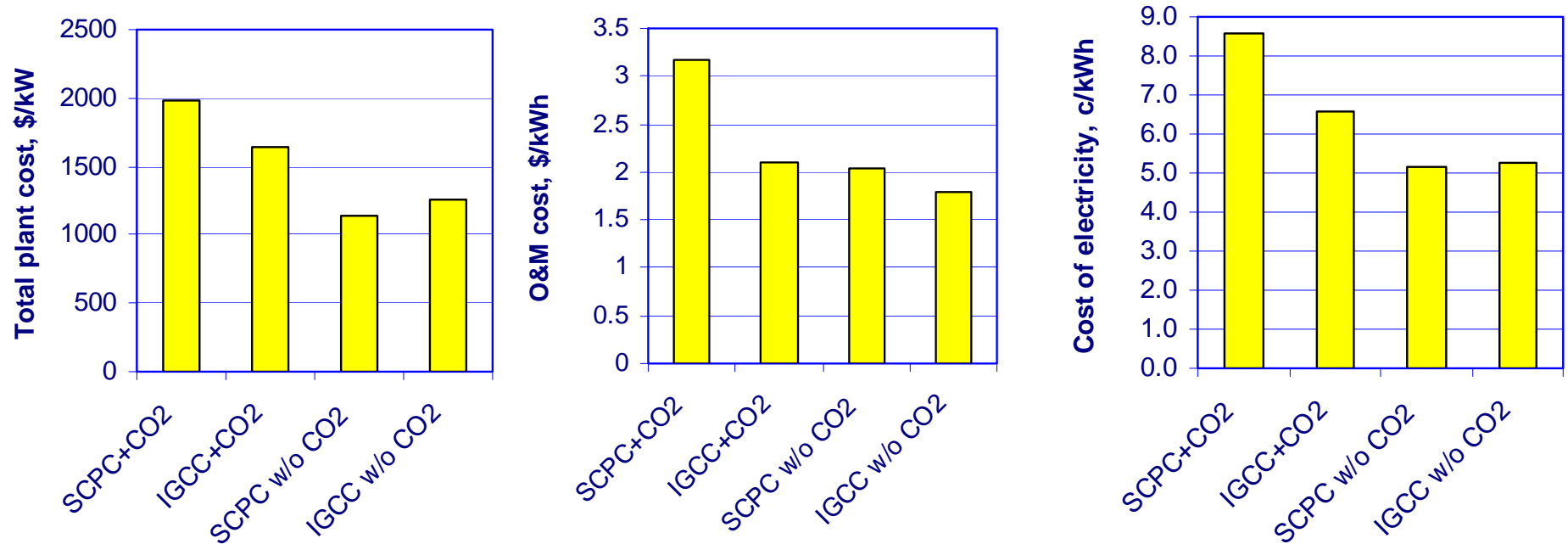
\* *without CO<sub>2</sub> removal*

\*\* *with CO<sub>2</sub> removal (MEA+SCPC, Selexol+IGCC)*

# Comparison between Super-Critical PC and IGCC



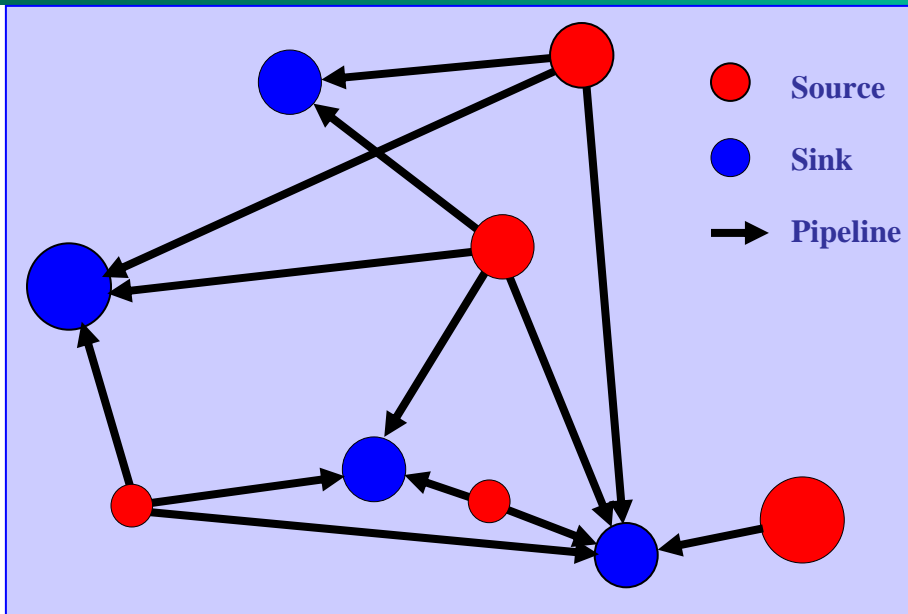
## Costs of capital, O&M and electricity



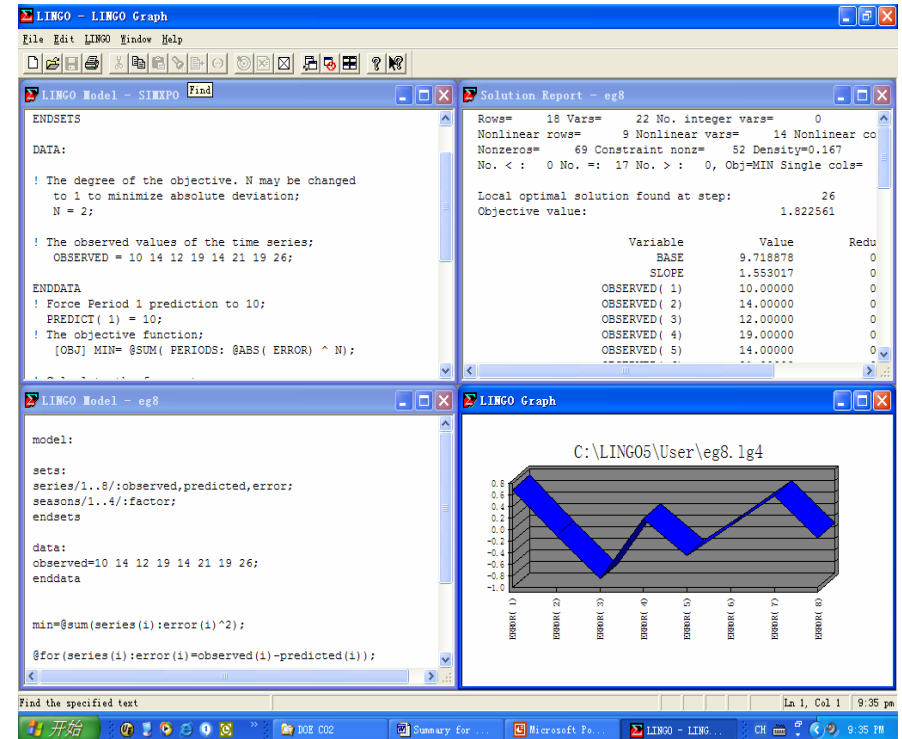
Based on assumptions : coal price of 1.24 MM Btu; 65% loading factor.

CO<sub>2</sub> avoidance costs: \$40-50 /metric ton CO<sub>2</sub> avoided for SCPC  
\$20-30 /metric ton CO<sub>2</sub> avoided for IGCC

# CO<sub>2</sub> Sequestration Optimization: Principles



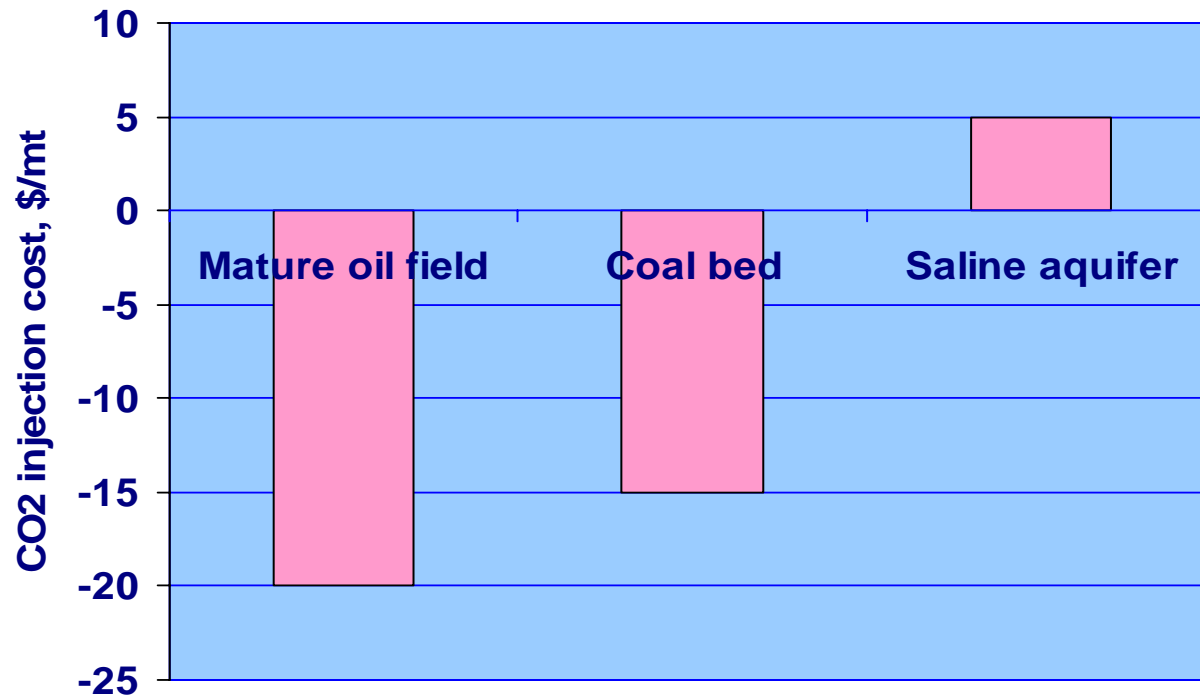
$$\begin{aligned}
 & \min \sum_i \sum_l R_i X_i (C_i + F_{il} C_{il} + F_{il} C_l) \\
 \text{st.} \quad & \begin{cases} \sum_i R_i X_i = R_{\text{target}} \\ X_i = \{0,1\}, \quad \forall i = 1, \dots, 122 \\ \sum_l F_{il} = 1, \quad \forall i = 1, \dots, 122 \\ \sum_i R_i X_i F_{il} \leq \text{Cap}_l, \quad \forall l = 1, \dots, 24 \\ F_{il} \geq 0, \quad \forall i = 1, \dots, 122; l = 1, \dots, 24 \end{cases}
 \end{aligned}$$



↑  
Lingo: Non-linear optimization software tool

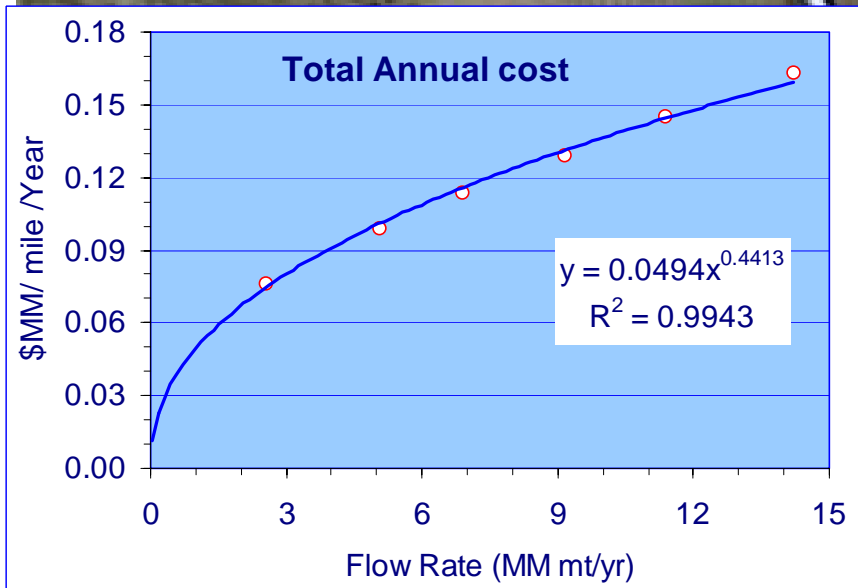
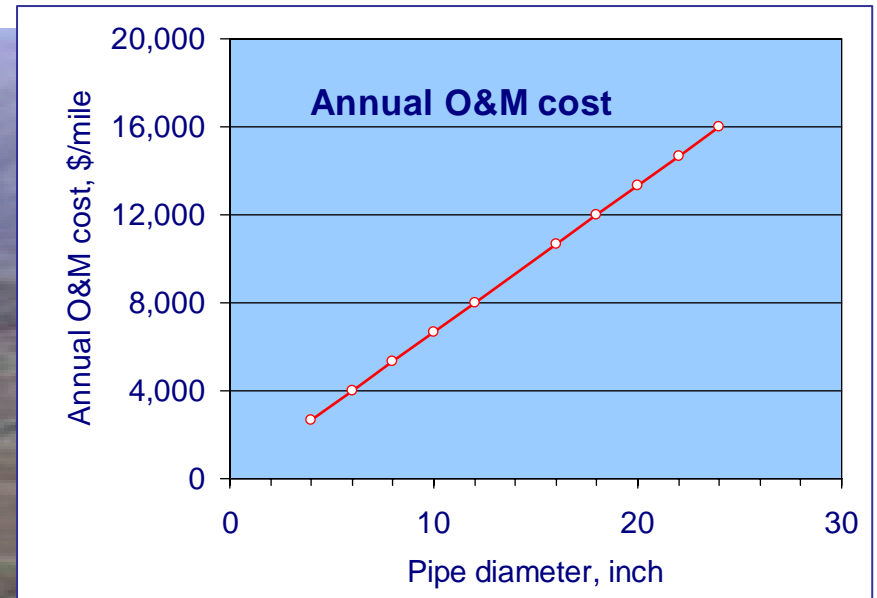
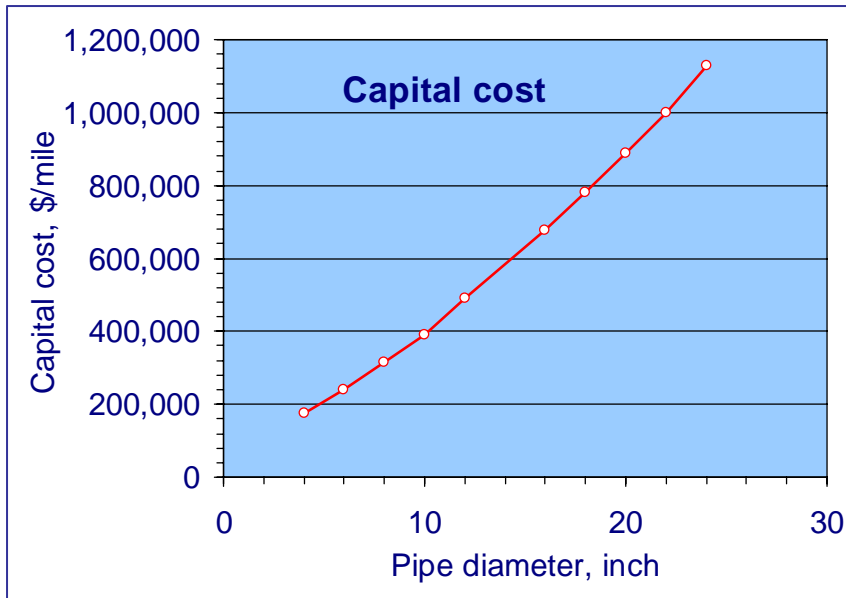
← Mathematical model

# Geological Storage Costs



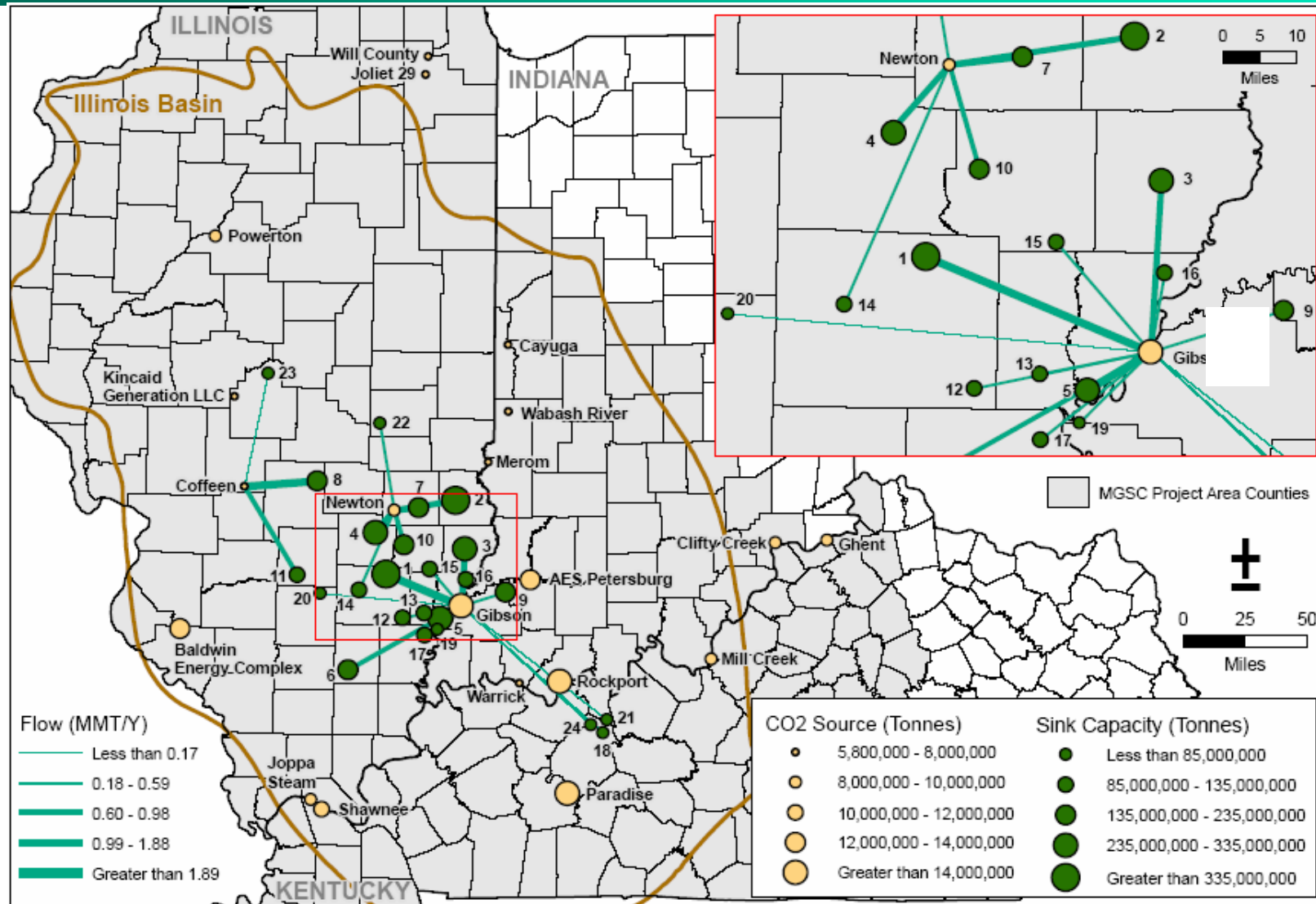
- ❑ *Saline aquifer*: \$5/mt CO<sub>2</sub>
- ❑ *Coal bed*: \$15/mt CO<sub>2</sub> credit for enhanced coal-bed methane recovery
- ❑ *Mature oil field*: \$20/mt CO<sub>2</sub> credit for enhanced oil recovery (corresponding to an oil price of \$25/barrel)

# Pipeline Transportation



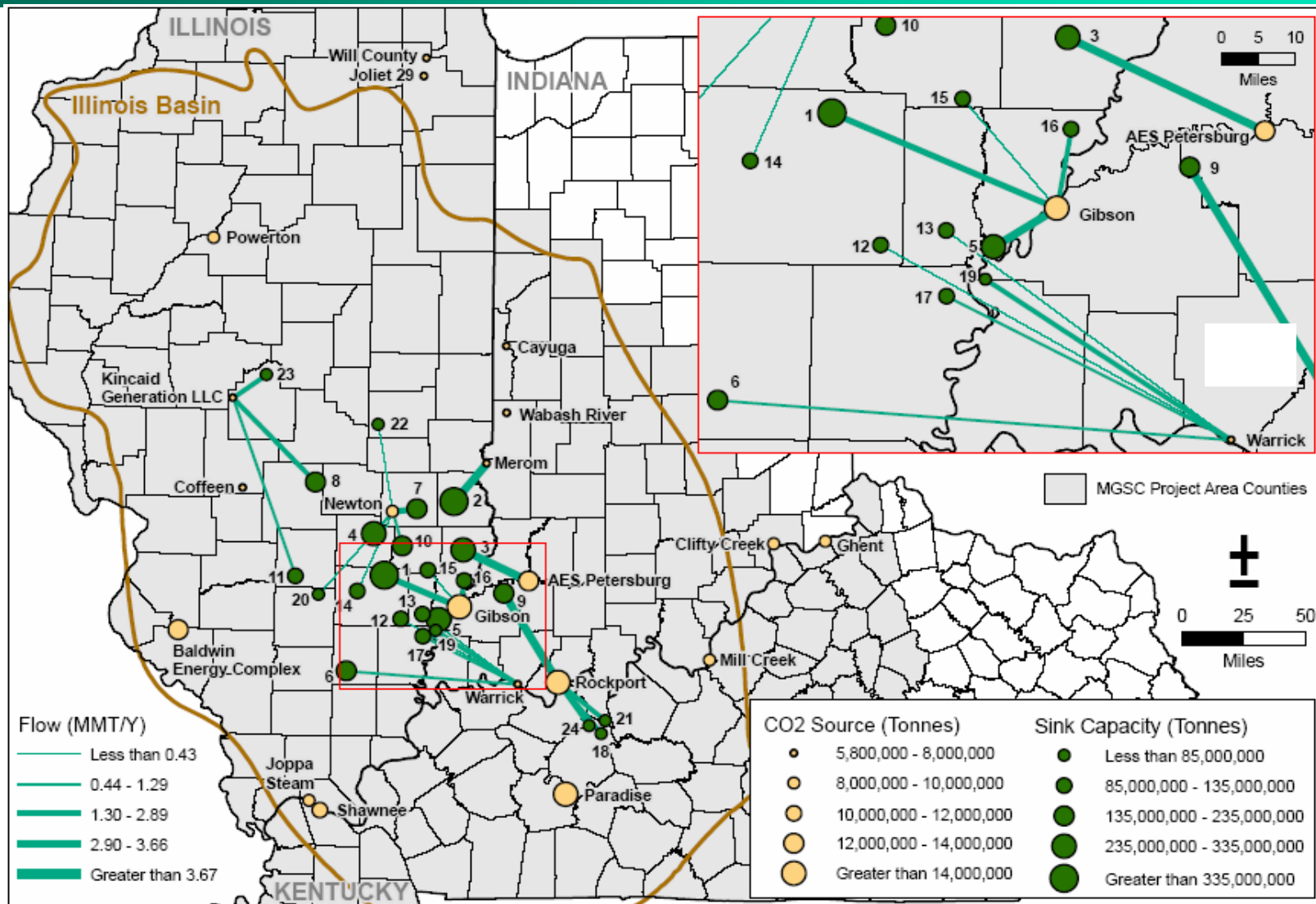
- Total annual cost = annualized capital cost + O&M cost
- Capital cost annualized by 13.05%/year
- Pipe diameter correlated with flow rate

# 10% Reduction



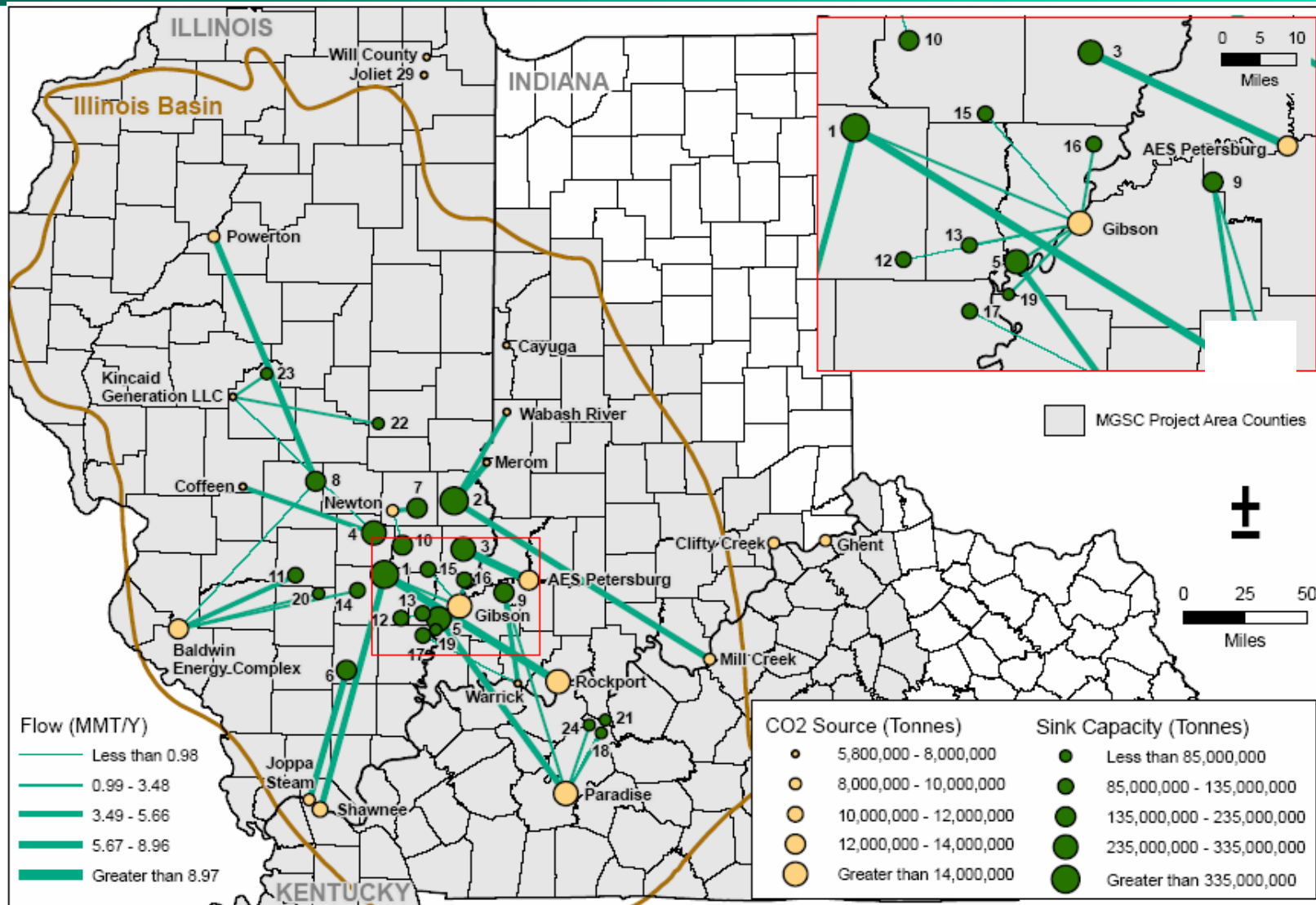
- ❑ 3 power plants, 27 MM mt/y CO<sub>2</sub> reduction, ~1634 MW electricity loss
- ❑ 17% of storage capacity including all EOR and ECBM
- ❑ Average pipeline distance 22.61 miles

# 25% Reduction



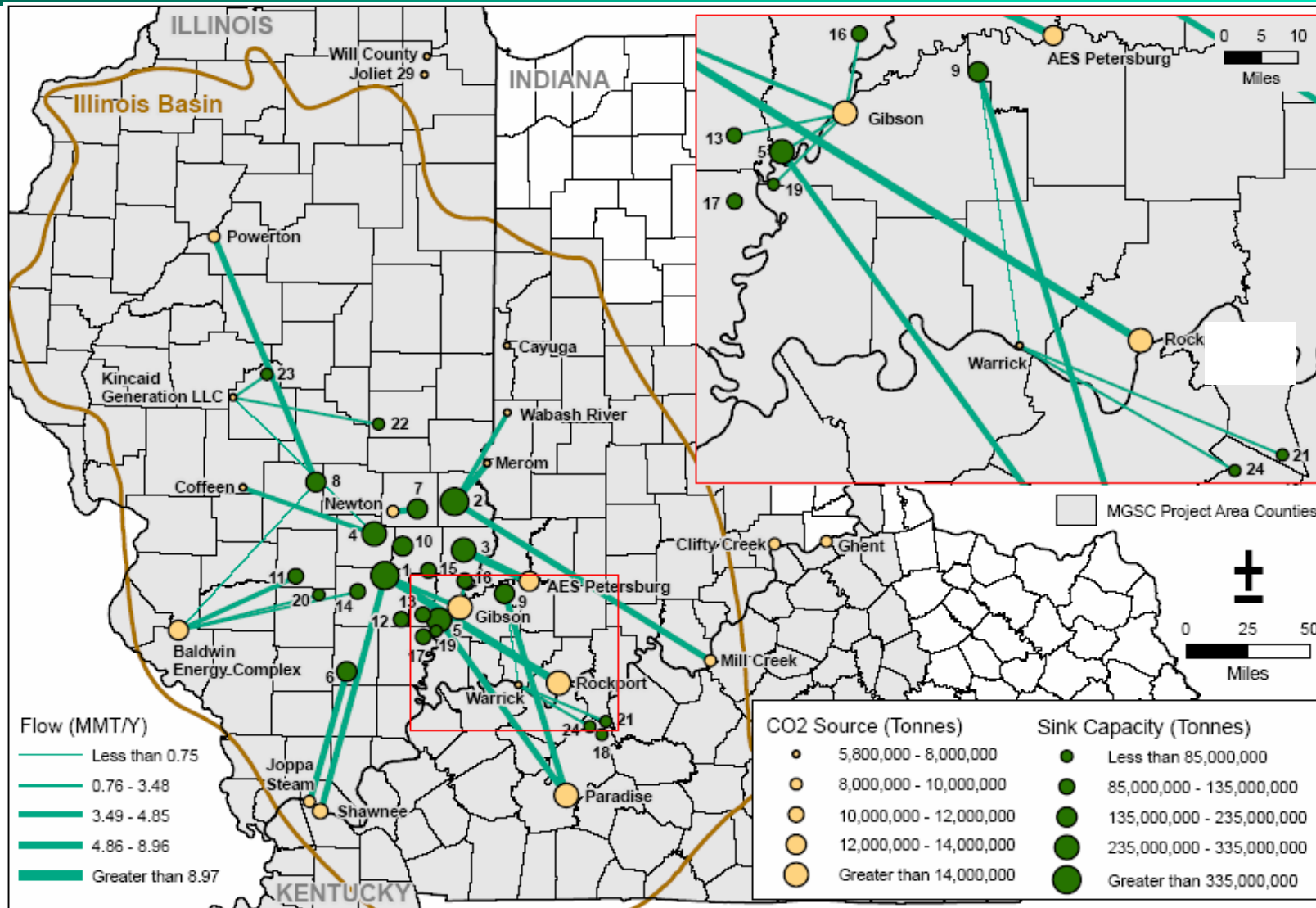
- ❑ 7 power plants, 64 MM mt/y CO<sub>2</sub> reduction , ~3873 MW electricity loss
- ❑ 41% of storage capacity including all EOR and ECBM
- ❑ Average pipeline distance 26.68 miles

# 50% Reduction



- ❑ 15 power plants, 128 MM mt/y CO<sub>2</sub> reduction , ~7746 MW electricity loss
- ❑ 82% of storage capacity including all EOR and ECBM
- ❑ Average pipeline distance 57.37 miles

# 50% Reduction without EOR and ECBM benefits



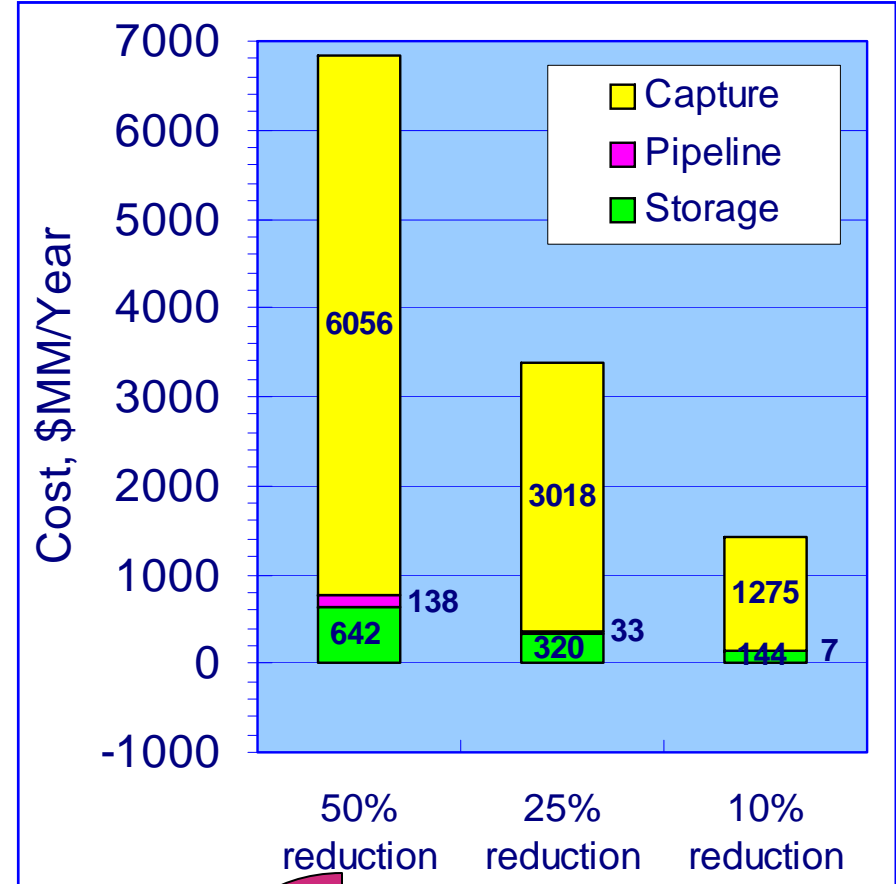
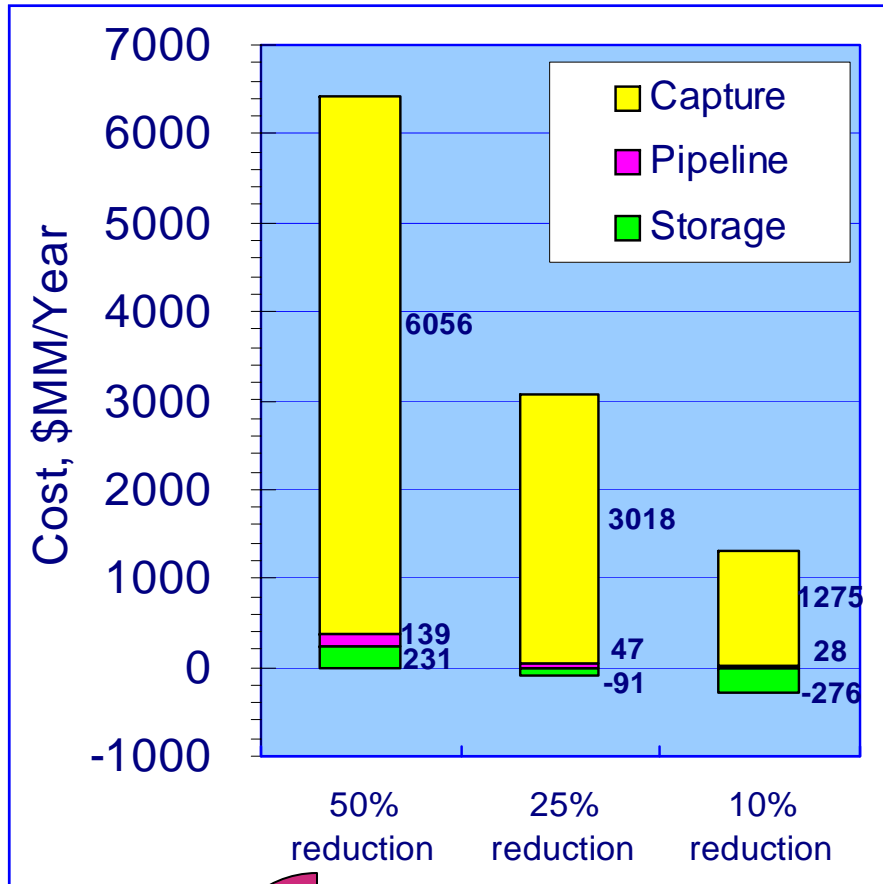
- ❑ No impacts on power plant selection and electricity loss
- ❑ 20 sinks, 82% of storage capacity
- ❑ Average pipeline distance 59.52 miles

# Cost Comparison: Annual Total Cost (\$MM/Year)

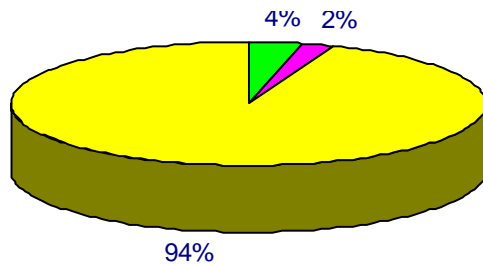


With EOR/ECBM credits

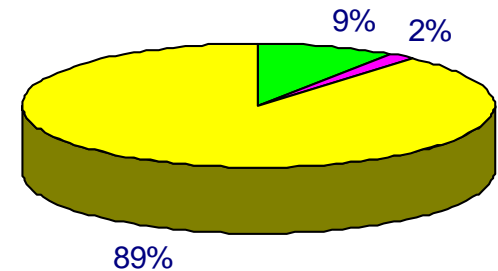
Without EOR/ECBM credits



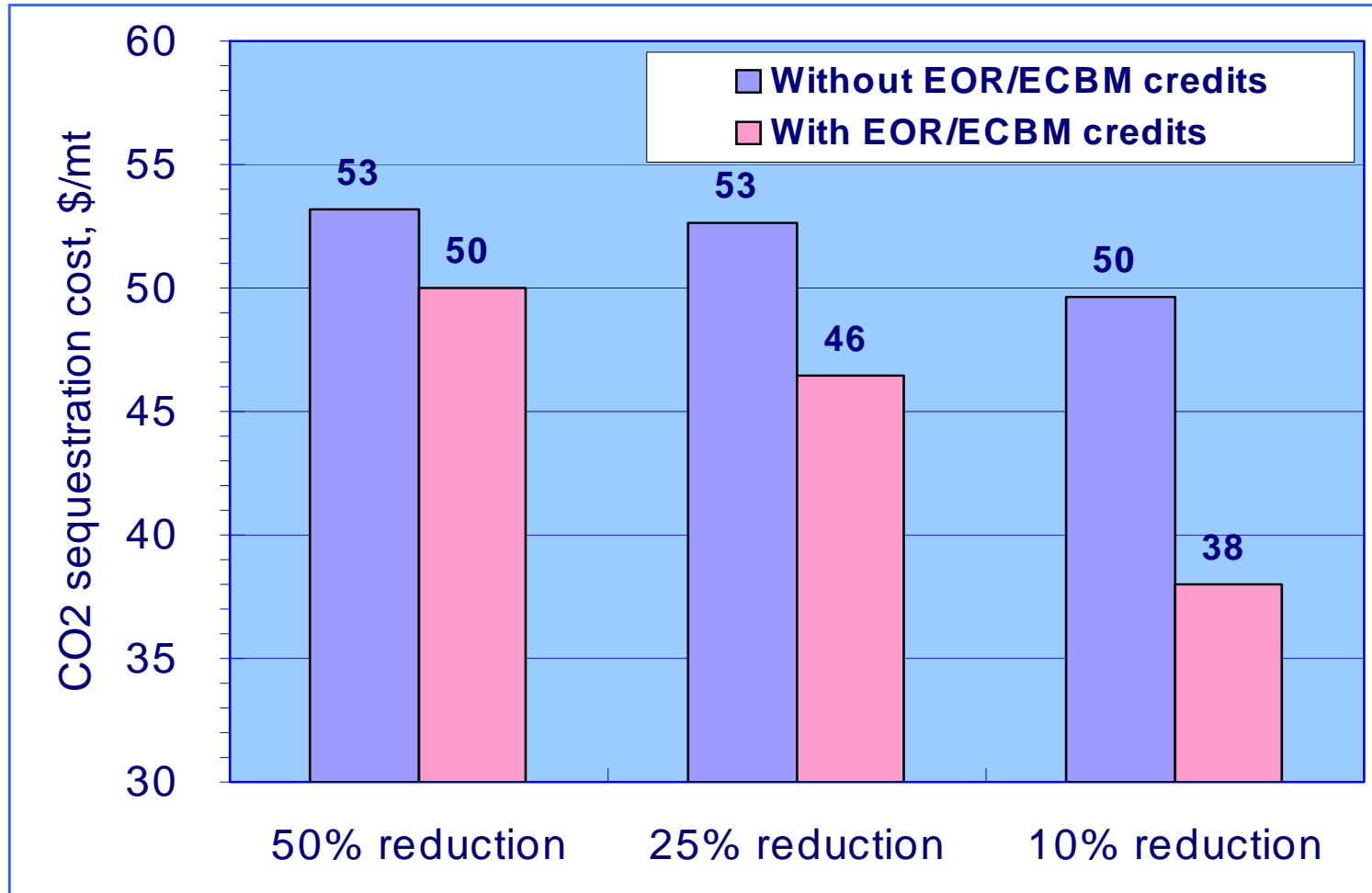
Cost distribution



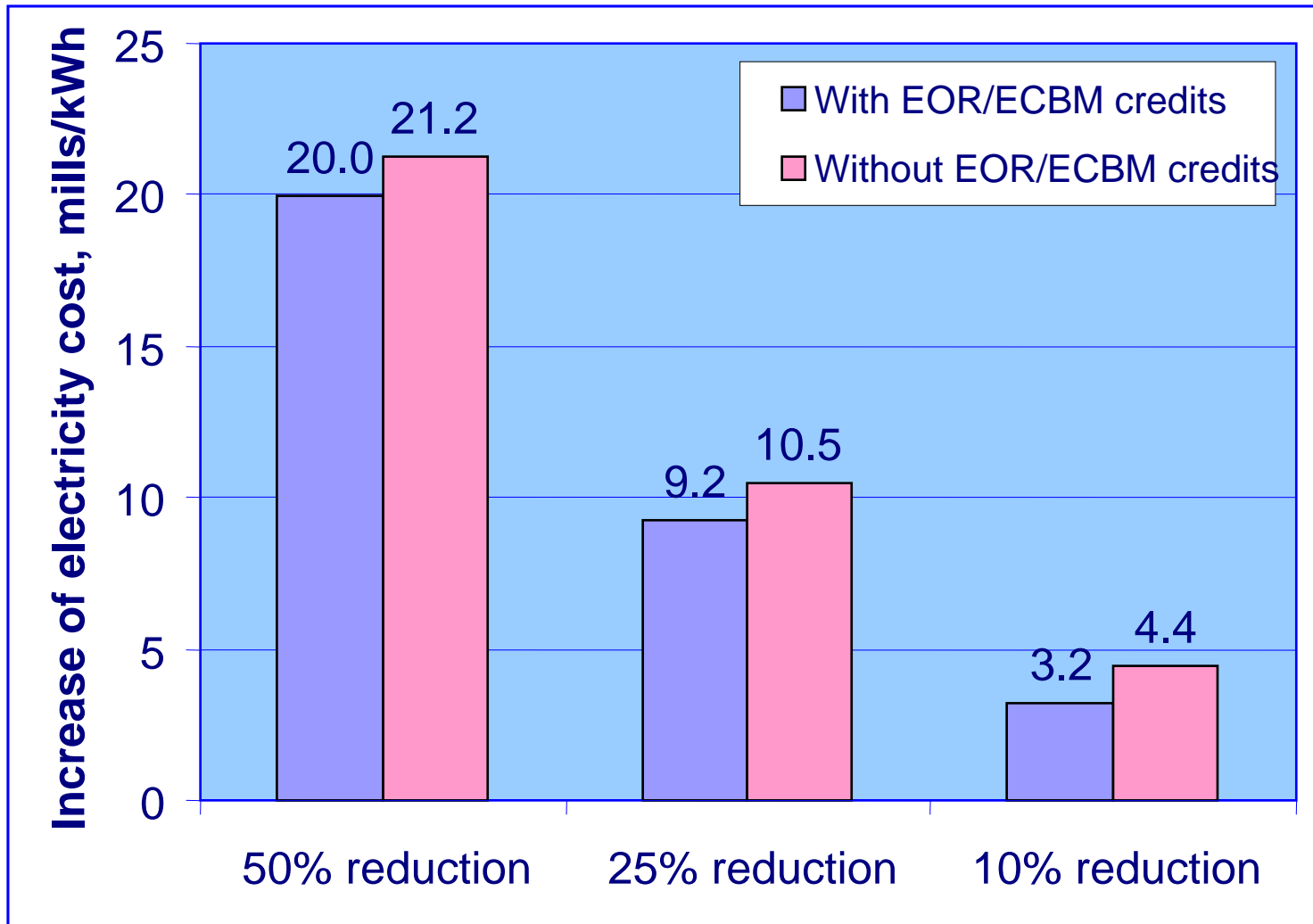
Cost distribution



# CO<sub>2</sub> Sequestration Cost (\$/mt)

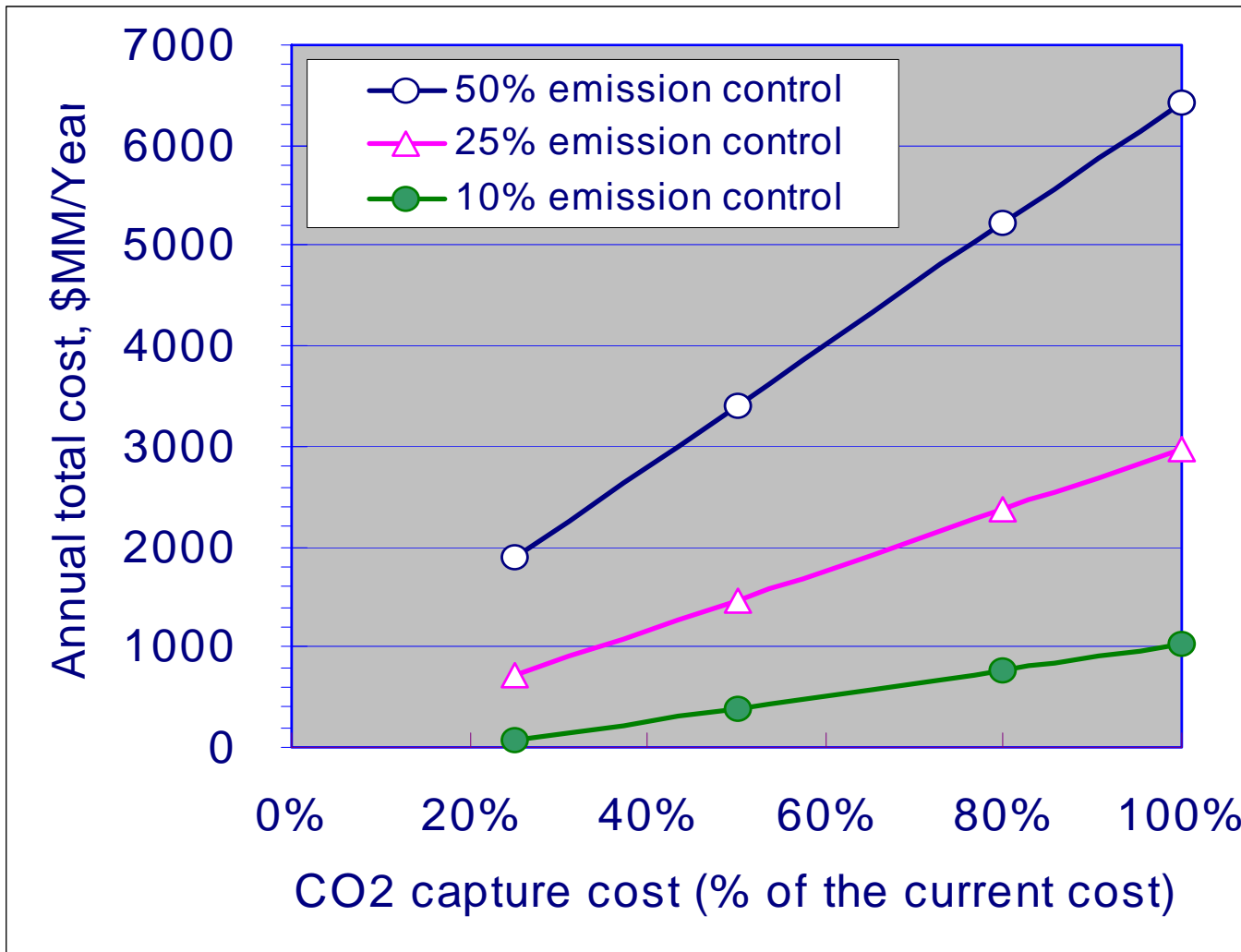


# Increase in Electricity Cost (mills/kWh)



Sequestration costs are shared by all utilities in the Basin

# Impact of CO<sub>2</sub> Capture Cost



# Summaries

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- ❑ *CO<sub>2</sub> capture cost generally contributes about 70-90% of sequestration system*
- ❑ *Absorption process is currently most feasible option for post-combustion CO<sub>2</sub> capture*
- ❑ *Current amine-based absorption processes are expensive (\$40-60/t CO<sub>2</sub> avoided) and energy intensive (30% loss of electricity output)*
- ❑ *Oxy-combustion is potentially attractive for retrofits of existing plants (commercial demonstration is required)*
- ❑ *Membrane and physical absorption processes are economically attractive for CO<sub>2</sub> capture in IGCC*

## Summaries (continued)

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- ❑ *CO<sub>2</sub> capture from large power plants is generally more economically attractive*
- ❑ *CO<sub>2</sub> storage in EOR and ECBM fields are economically preferred regardless of their locations in the Basin*
- ❑ *Sequestration cost ranges from \$38 to \$50/mt CO<sub>2</sub> for 10% to 50% control levels*
- ❑ *Sequestration cost significantly decreases at 10% control level if benefits from EOR and ECBM are included*



*Thank you !*